

CEDA DREDGING TECHNOLOGY WEBINARS #6

WELCOME

Flow regime diagrams in slurry transport models

Dr. ir. Sape Miedema

Delft University of Technology



DHLLDV Framework Flow Regimes & Scenarios

**Dr.ir. Sape A. Miedema
Head of Studies**

**MSc Offshore & Dredging Engineering
& Marine Technology
&**

**Associate Professor of
Dredging Engineering**

Delft University of Technology



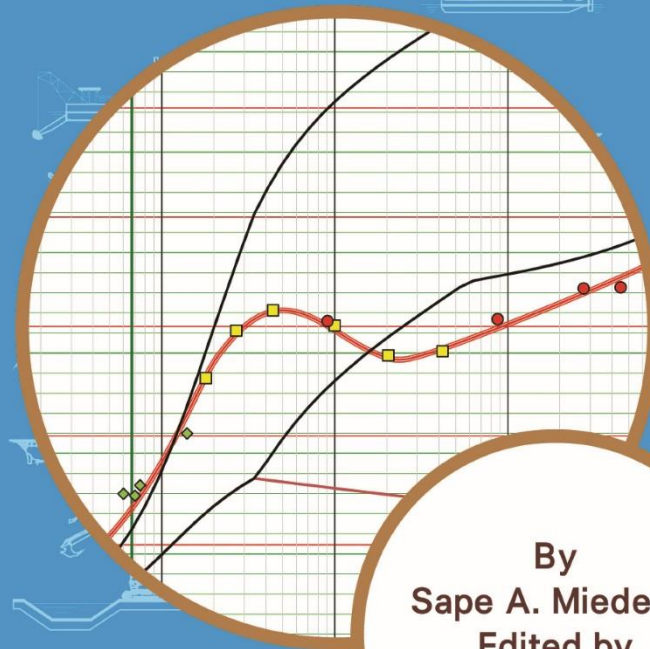


Dredging A Way Of Life



SLURRY TRANSPORT

Fundamentals, A Historical Overview
& The Delft Head Loss & Limit
Deposit Velocity Framework



By
Sape A. Miedema
Edited by
Robert C. Ramsdell



Introduction

Chapter 7.1

The Elephant of Wilson



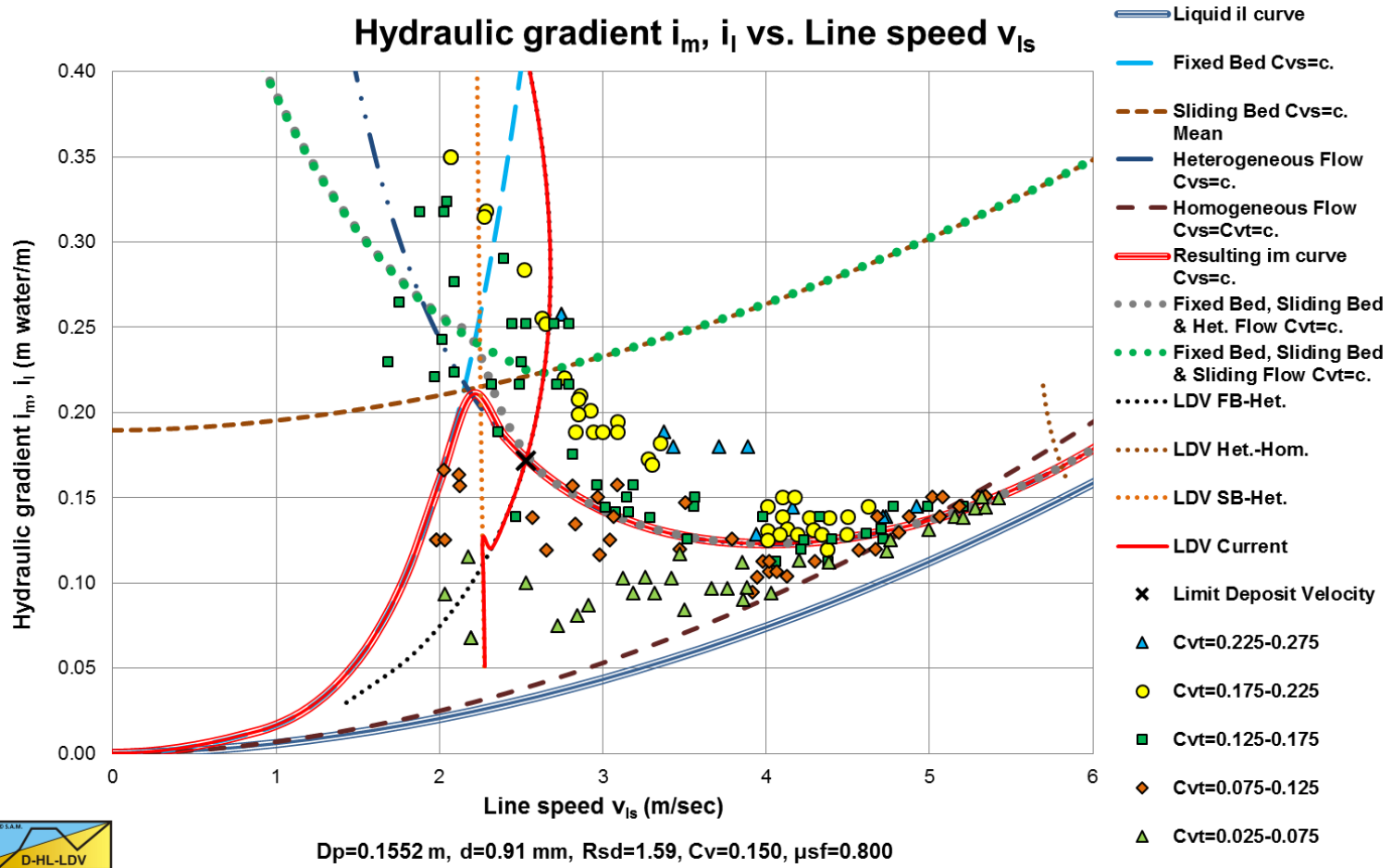
Possibilities

- 1. Small versus large pipe diameter**
- 2. Small versus large particle diameter**
- 3. Low versus high concentration**
- 4. Low versus high line speed**
- 5. Spatial versus delivered concentration**
- 6. Uniform versus graded sands/gravels**

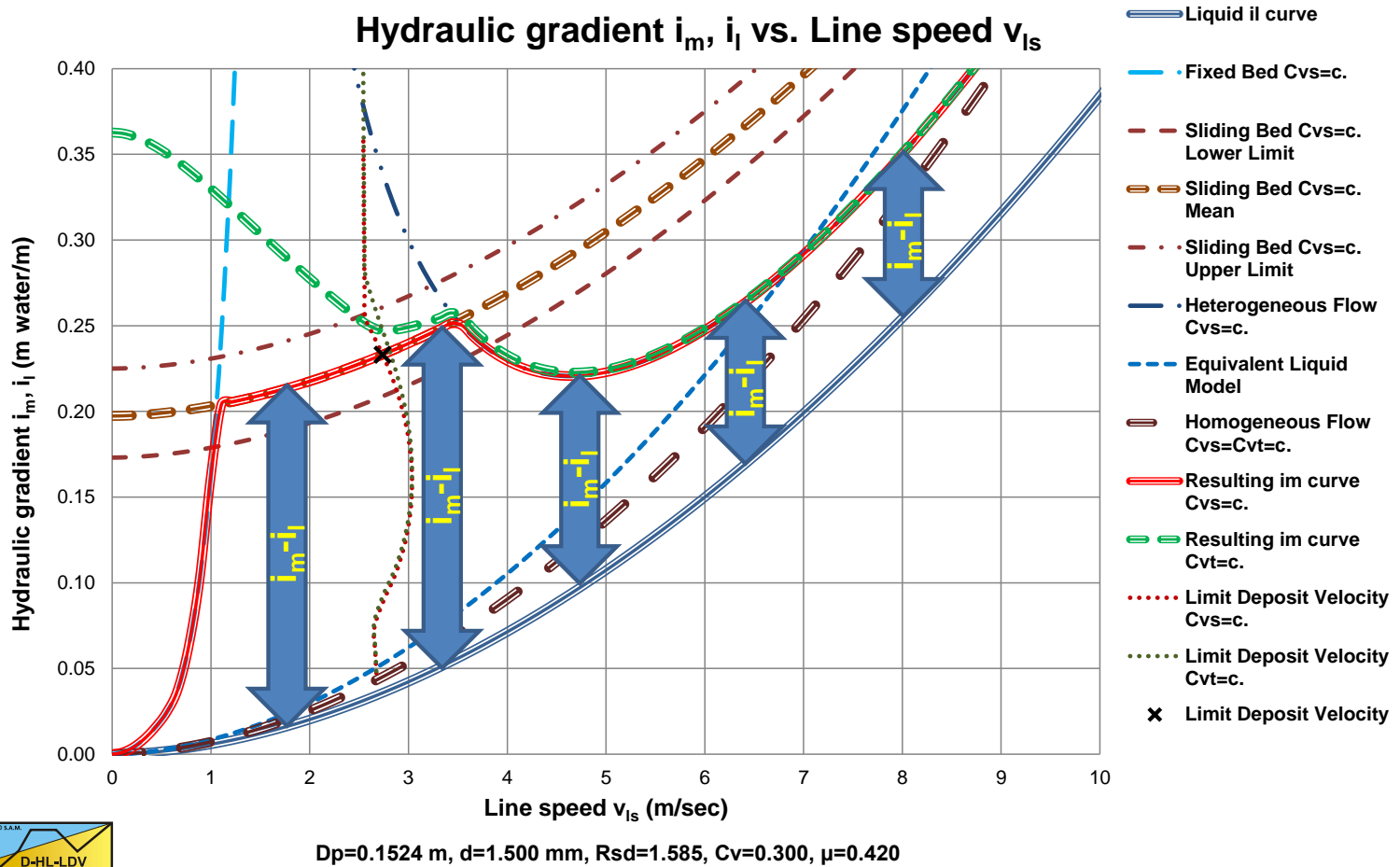
- 1. Carrier liquid properties**
- 2. Solids properties**

For sands/gravels in water 64 combinations possible

Data from Yagi et al., C_{vs}



DHLLDV Model, The Solids Effect, C_{vs}

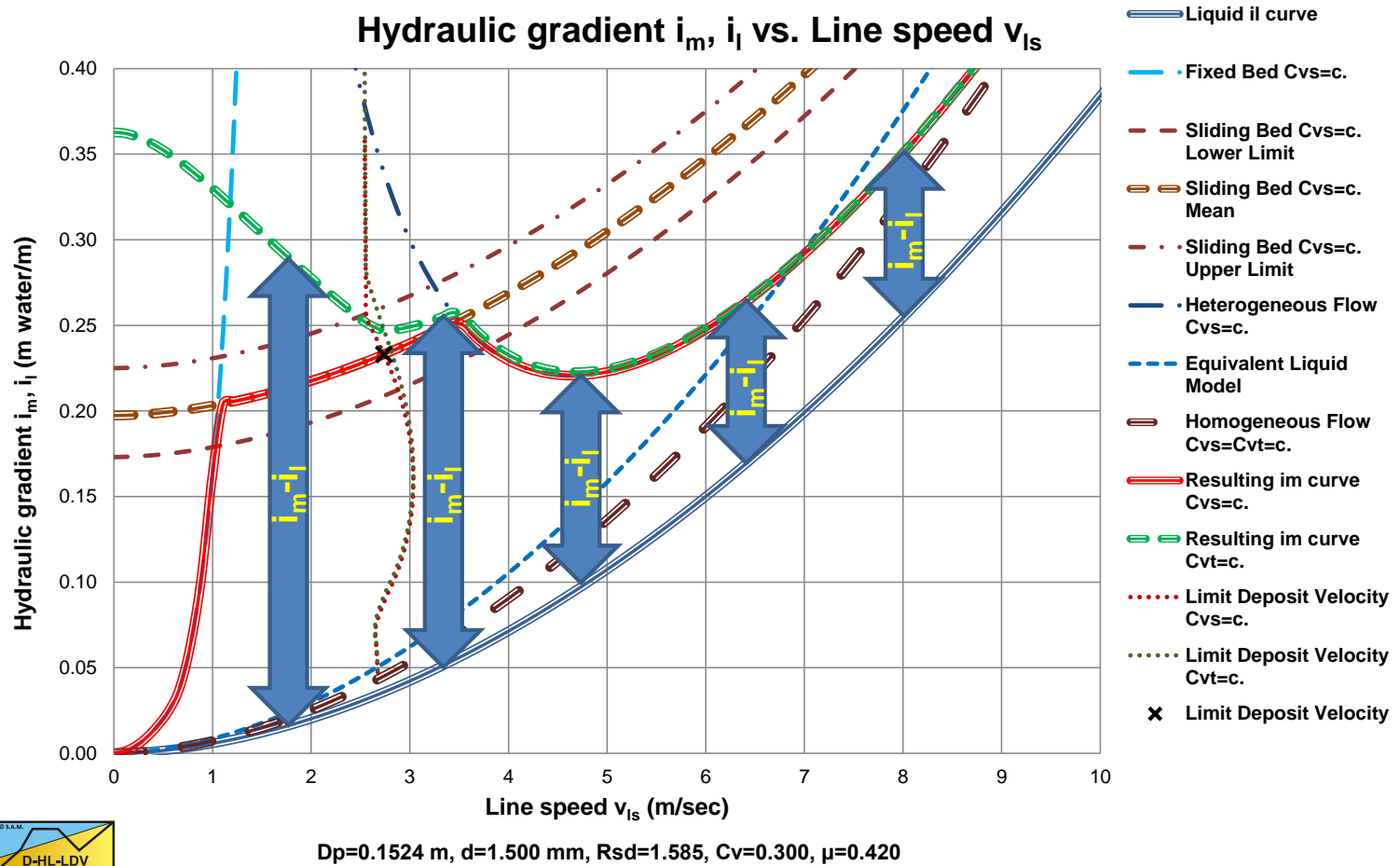


$$i_l = \frac{\Delta p_l}{\rho_l \cdot g \cdot \Delta L} = \frac{\lambda_l \cdot v_{ls}^2}{2 \cdot g \cdot D_p}$$

$$E_{rhg} = \frac{i_m - i_l}{R_{sd} \cdot C_v}$$

Delft University of Technology – Offshore & Dredging Engineering

DHLLDV Model, The Solids Effect, C_{vt}



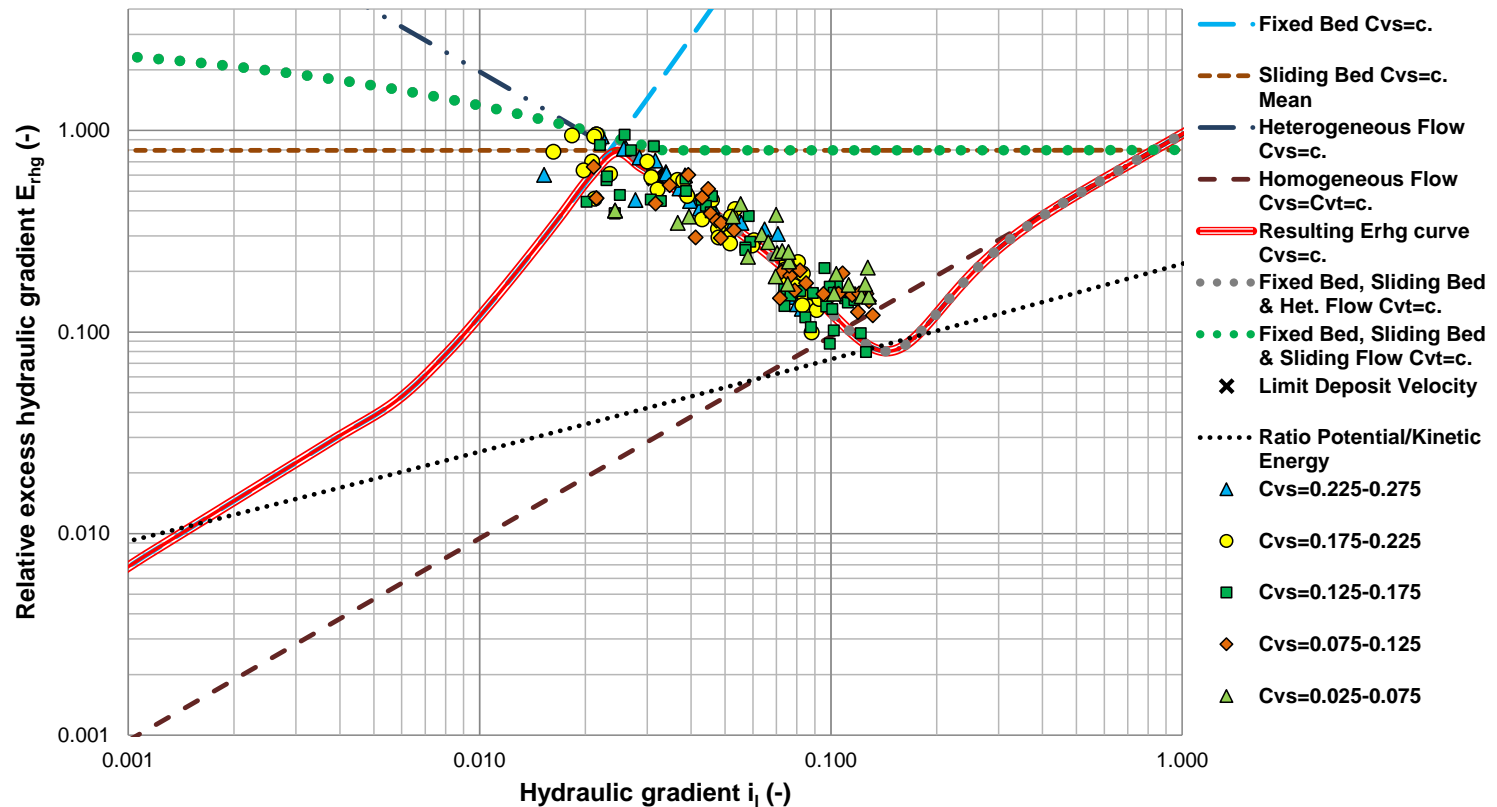
$$i_l = \frac{\Delta p_l}{\rho_l \cdot g \cdot \Delta L} = \frac{\lambda_l \cdot v_{ls}^2}{2 \cdot g \cdot D_p}$$

$$E_{rhg} = \frac{i_m - i_l}{R_{sd} \cdot C_v}$$

Delft University of Technology – Offshore & Dredging Engineering

Data from Yagi et al., C_{vs}

Relative excess hydraulic gradient E_{rhg} vs. Hydraulic gradient i_i



$D_p=0.1552$ m, $d=0.91$ mm, $R_{sd}=1.59$, $C_v=0.150$, $\mu_{sf}=0.800$

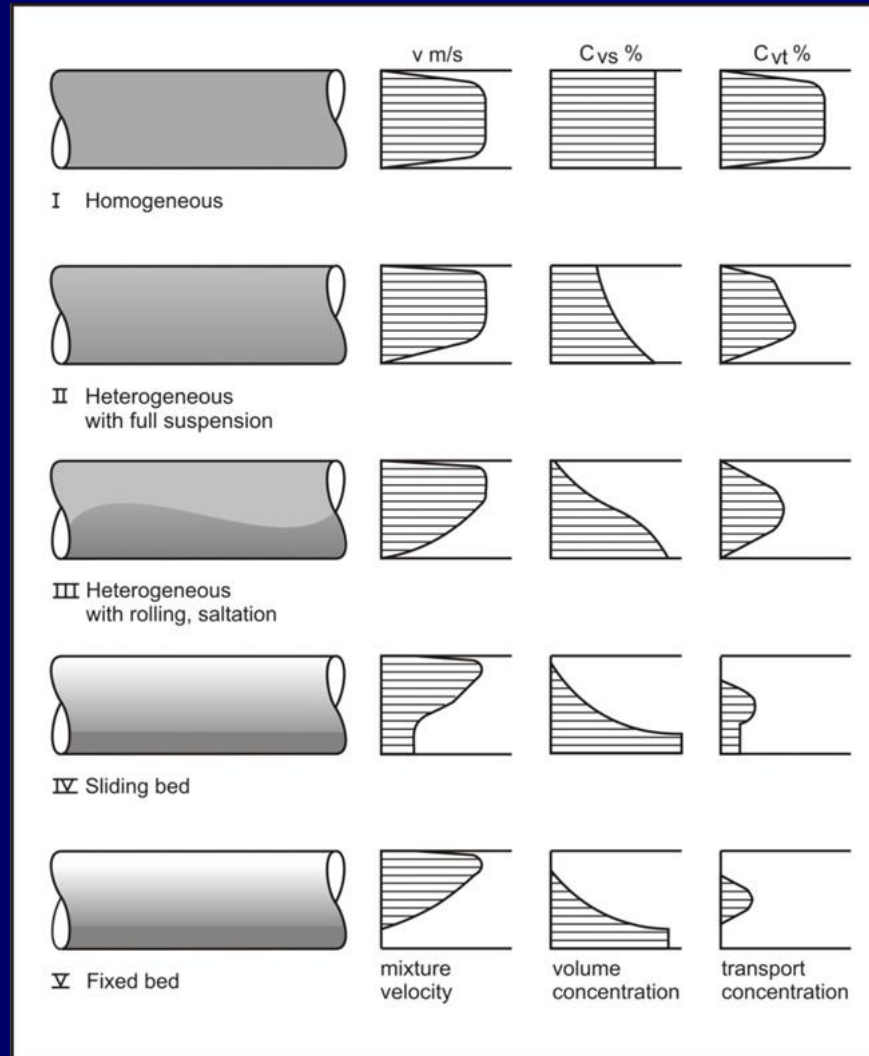




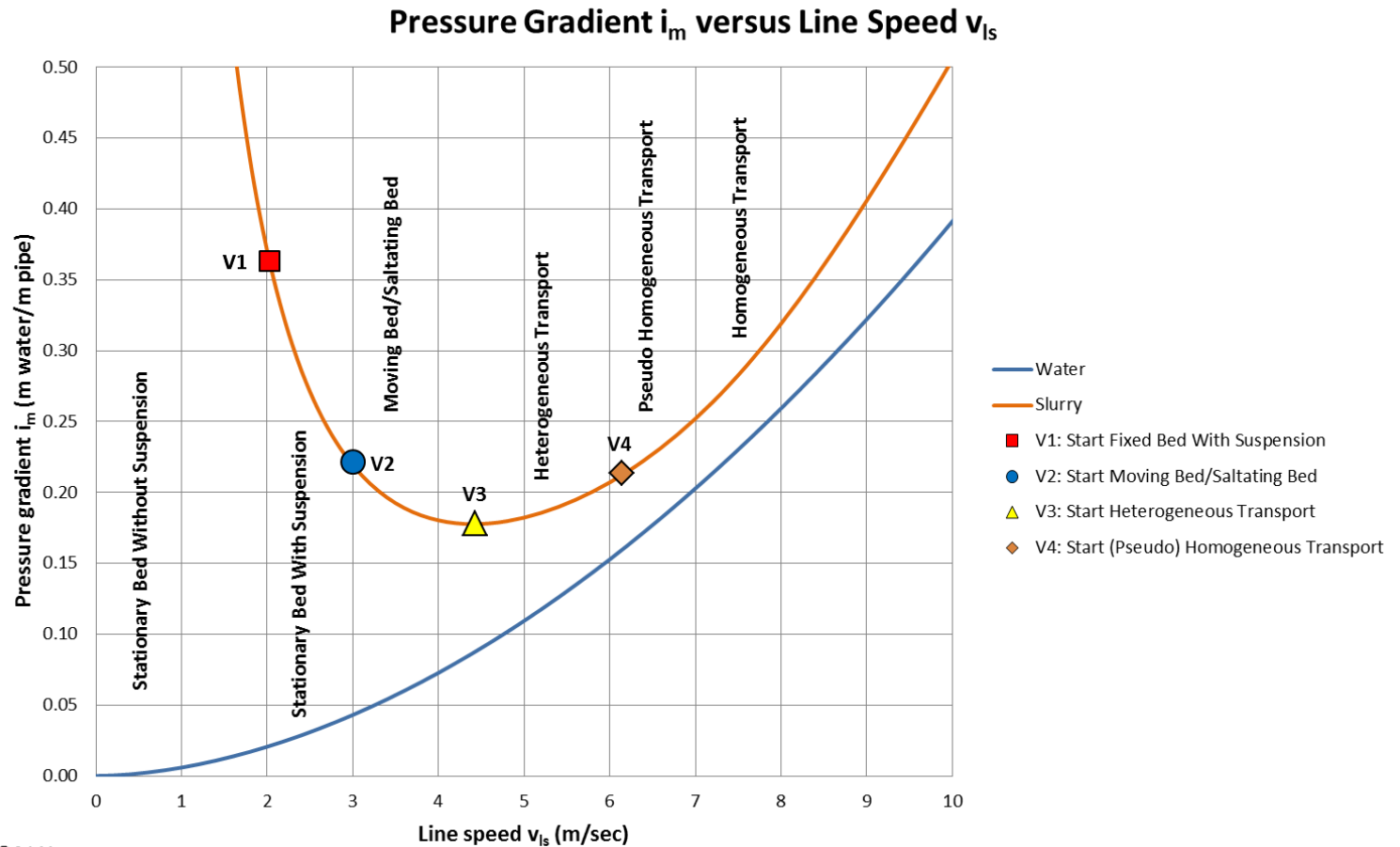
Regimes History

Chapter 1

Regimes History



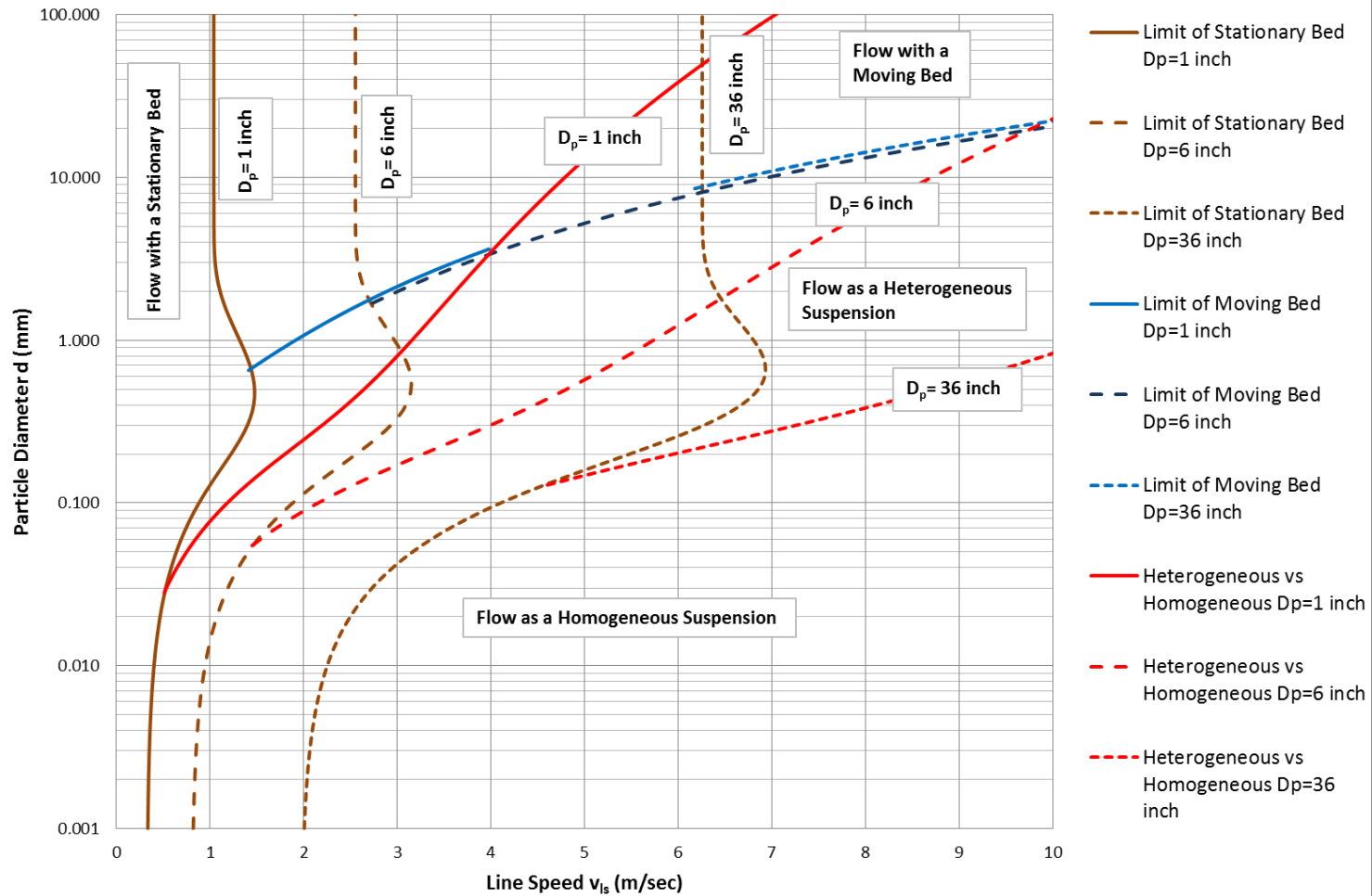
Abulnaga (2002)



© S.A.M.

Newitt/Miedema (2013)

Flow Regimes according to Newitt et al. (1955) & Durand & Condolios (1952)



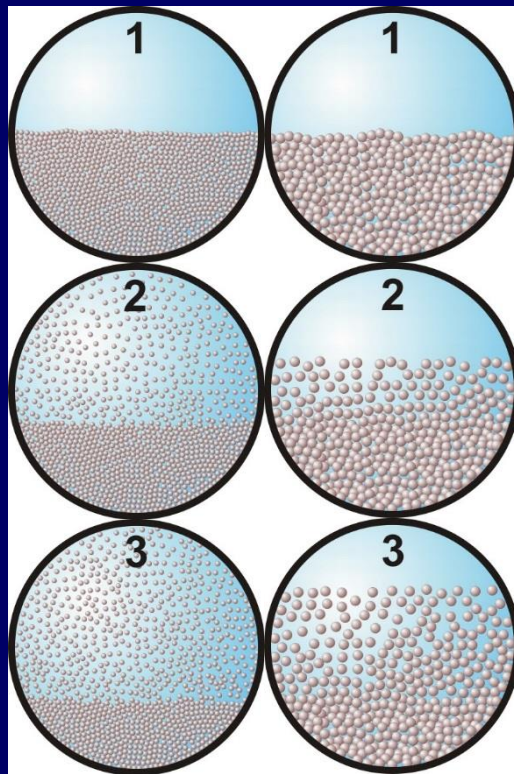
© S.A.M.



Flow Regimes

Chapter 7.2

Flow Regimes 1

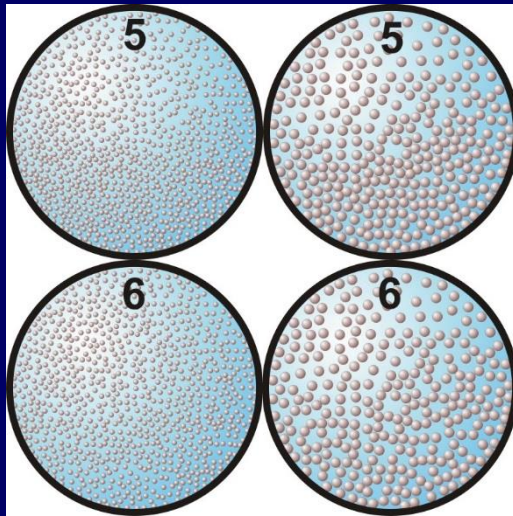


1: Fixed bed without suspension or sheet flow, constant C_{vs} .

2: Fixed bed with suspension or sheet flow, constant C_{vs} .

3: Fixed bed with suspension or sliding bed with sheet flow, constant C_{vs} .

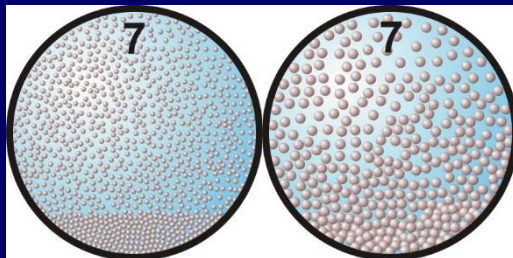
Flow Regimes 2



5: Heterogeneous transport,
 $C_{vt} \approx C_{vs}$

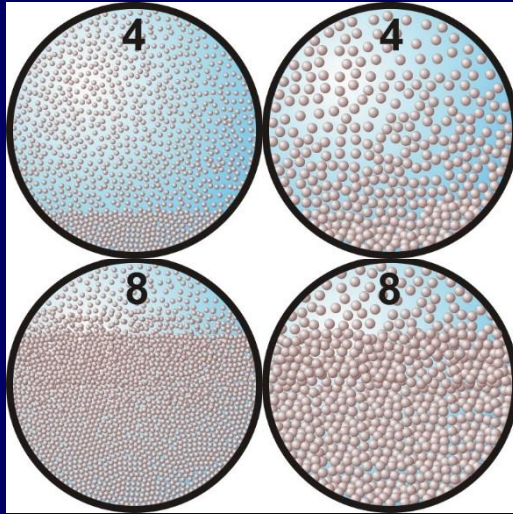
6: Homogeneous transport,
 $C_{vt} \approx C_{vs}$

5/6: Pseudo homogeneous
transport, $C_{vt} \approx C_{vs}$



7: Sliding Flow if $d/D_p > 0.015$.

Flow Regimes 3



4: Fixed bed with suspension or sliding bed with sheet flow, constant C_{vt} .

8: Fixed bed with suspension or sliding bed with sheet flow, constant C_{vt} .

Distinguish C_{vs} & C_{vt}

Scenario's with L are with C_{vs}

Scenario's with R are with C_{vt}



Scenarios

Chapter 7.2

Equations in Graphs

Hydraulic Gradient i

$$i_l = \frac{\Delta p_l}{\rho_l \cdot g \cdot L} \quad \text{or} \quad i_m = \frac{\Delta p_m}{\rho_l \cdot g \cdot L}$$

for water as carrier fluid:

$$\frac{\lambda_l \cdot \frac{\Delta L}{D_p} \cdot \frac{1}{2} \cdot \rho_l \cdot v_{ls}^2}{\rho_l \cdot g \cdot \Delta L} = \frac{\lambda_l \cdot v_{ls}^2}{2 \cdot g \cdot D_p}$$

Relative Submerged Density R_{sd}

$$R_{sd} = \frac{\rho_s - \rho_l}{\rho_l}$$

Relative Excess Hydraulic Gradient E_{rhg}

$$E_{rhg} = \frac{i_m - i_l}{R_{sd} \cdot C_{vs}} \quad \text{or} \quad E_{rhg} = \frac{i_m - i_l}{R_{sd} \cdot C_{vt}}$$

Spatial versus Transport Concentration & the Slip Velocity

Spatial Volumetric Concentration is volume based.
Transport Volumetric Concentration is volume flow based.

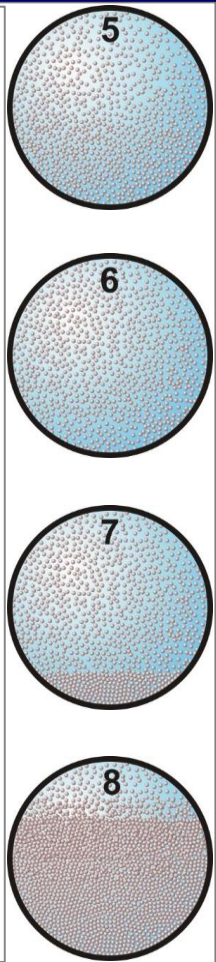
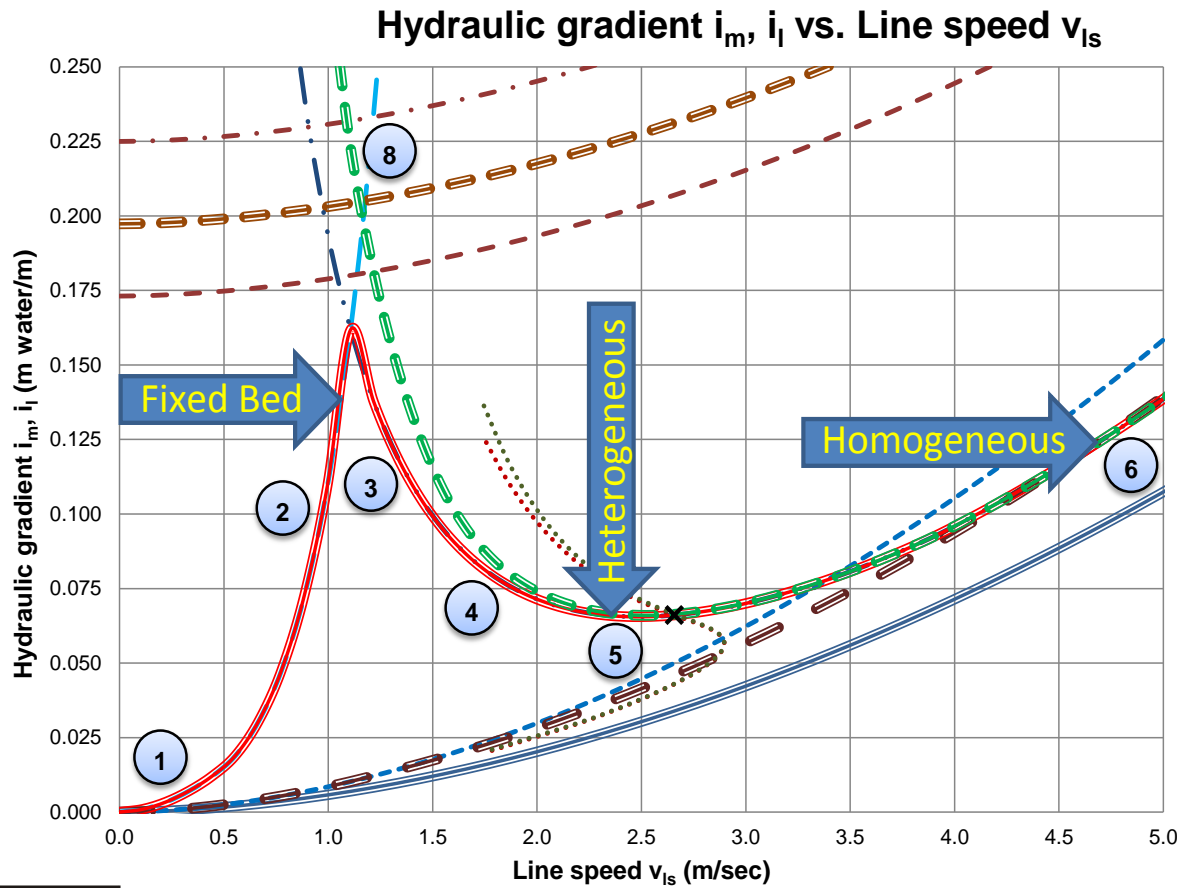
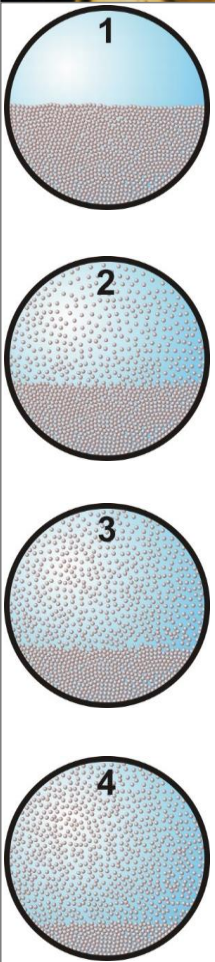
$$C_{vt} = \left(1 - \frac{v_{sl}}{v_{ls}} \right) \cdot C_{vs} \quad \Rightarrow \quad C_{vt} < C_{vs}$$

$$C_{vs} = \left(\frac{v_{ls}}{v_{ls} - v_{sl}} \right) \cdot C_{vt}$$

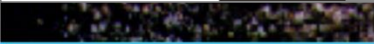
Relative Excess Hydraulic Gradient E_{rhg} , $C_{vt} = \text{constant}$

$$E_{rhg} = \frac{i_m - i_l}{R_{sd} \cdot \left(1 - \frac{v_{sl}}{v_{ls}} \right) \cdot C_{vs}} = \left(\frac{v_{ls}}{v_{ls} - v_{sl}} \right) \cdot \frac{i_m - i_l}{R_{sd} \cdot C_{vs}}$$

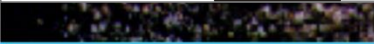
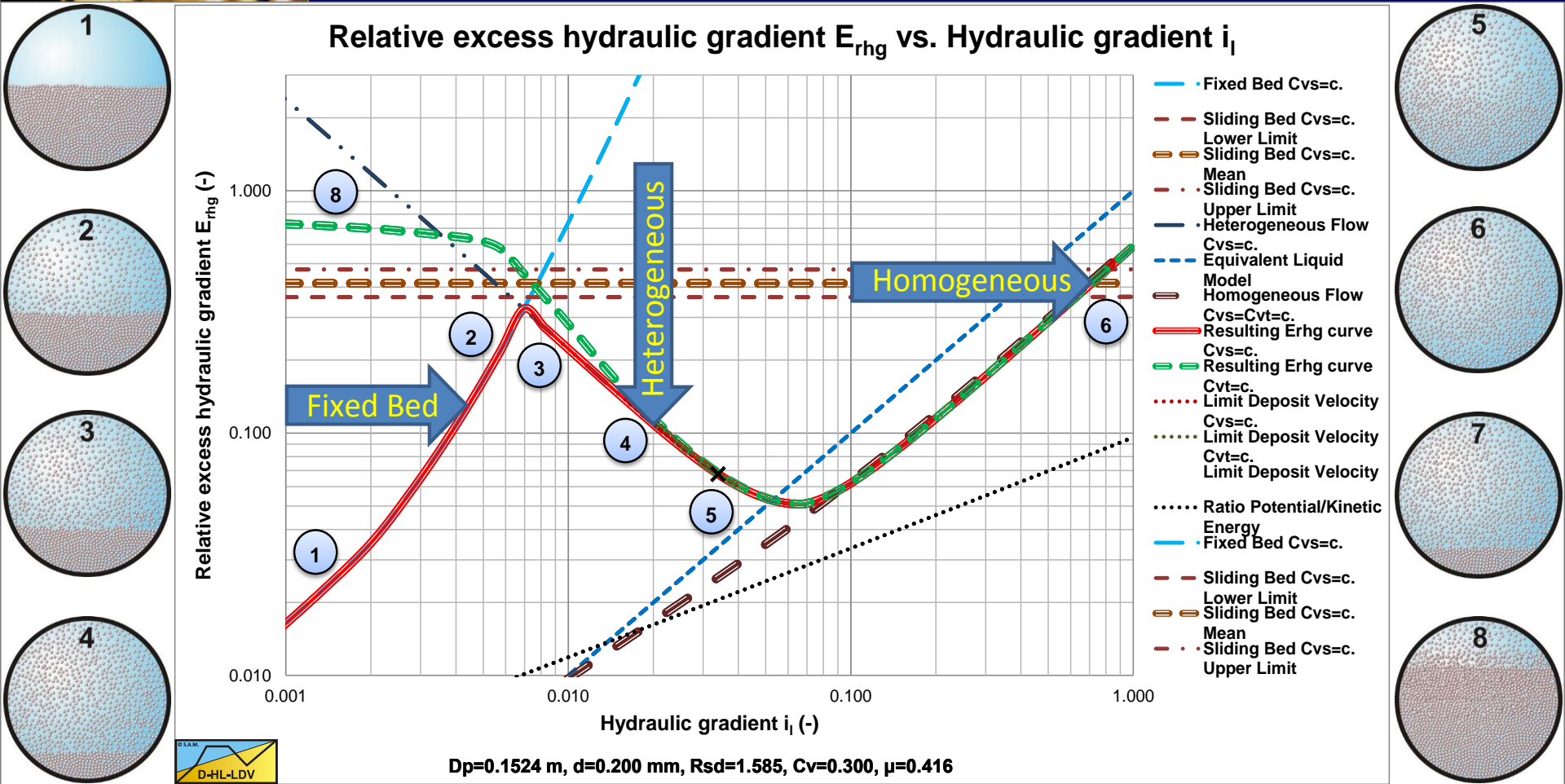
Scenario L1 & R1, $i_m - v_{Is}$



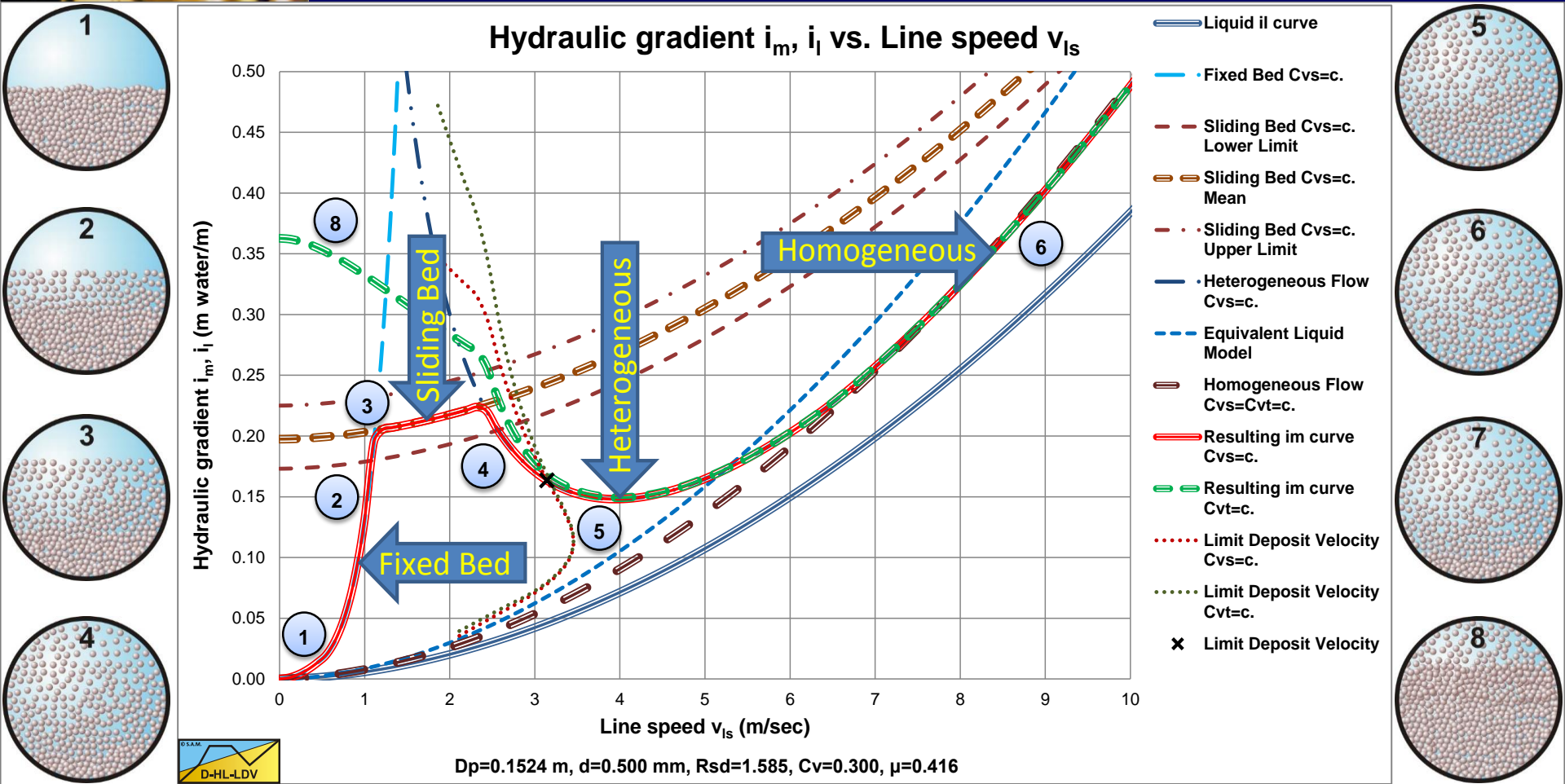
$D_p=0.1524 \text{ m}, d=0.200 \text{ mm}, Rsd=1.585, Cv=0.300, \mu=0.416$



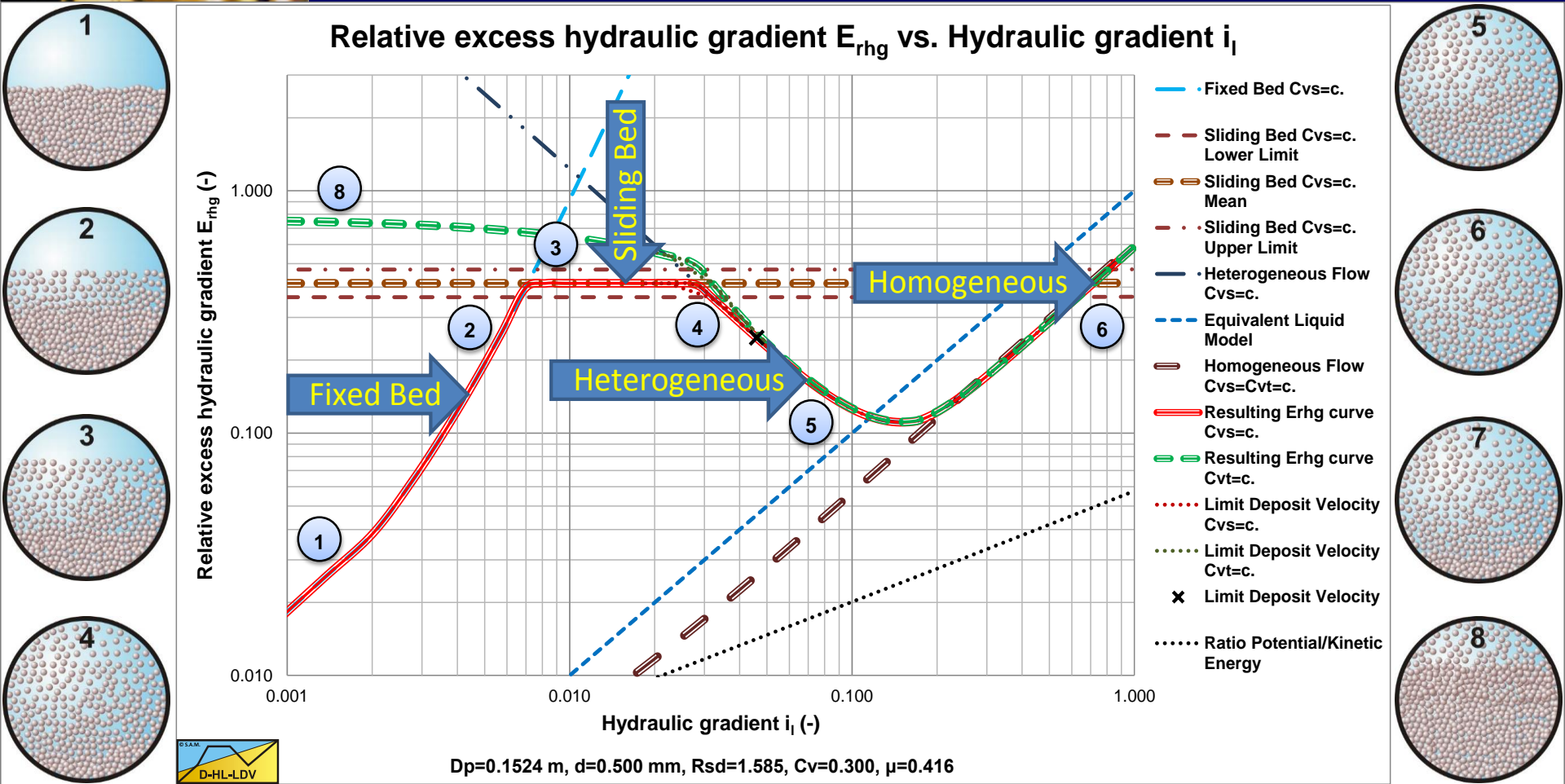
Scenario L1 & R1, $E_{rhg}-i_1$



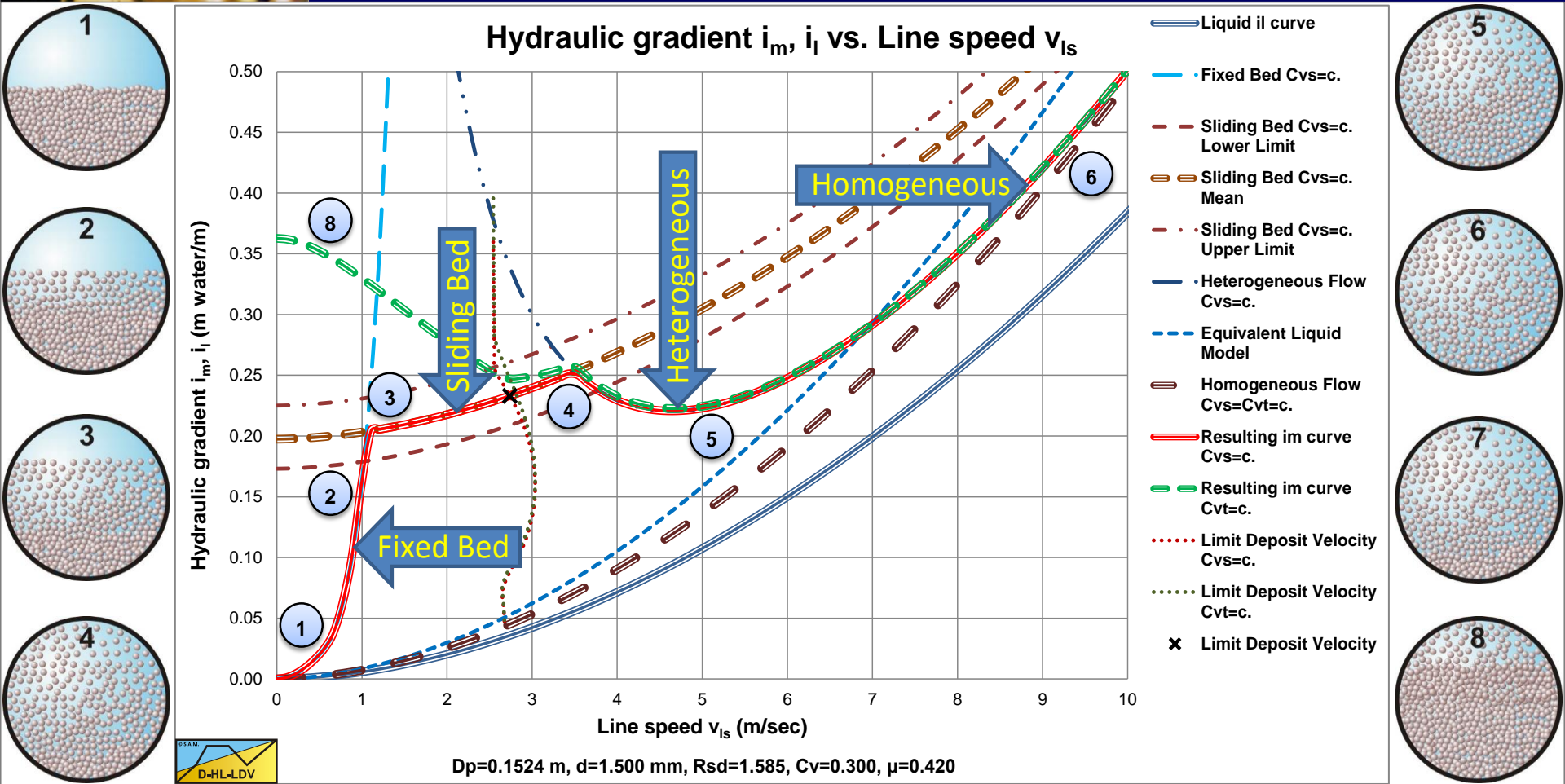
Scenario L2A & R2A, $i_m - v_{Is}$



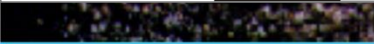
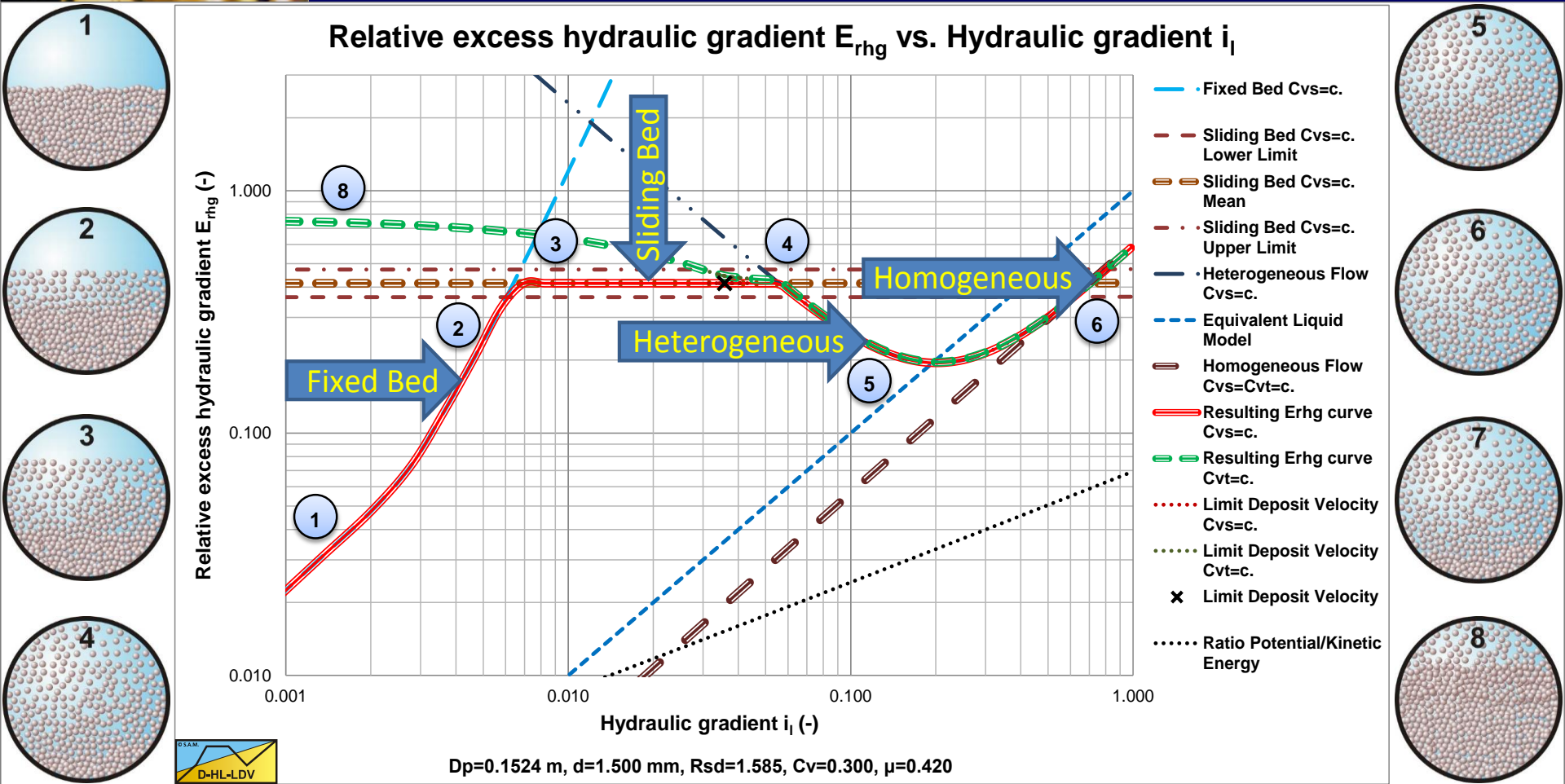
Scenario L2A & R2A, $E_{rhg}-i_1$



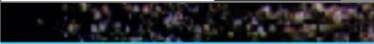
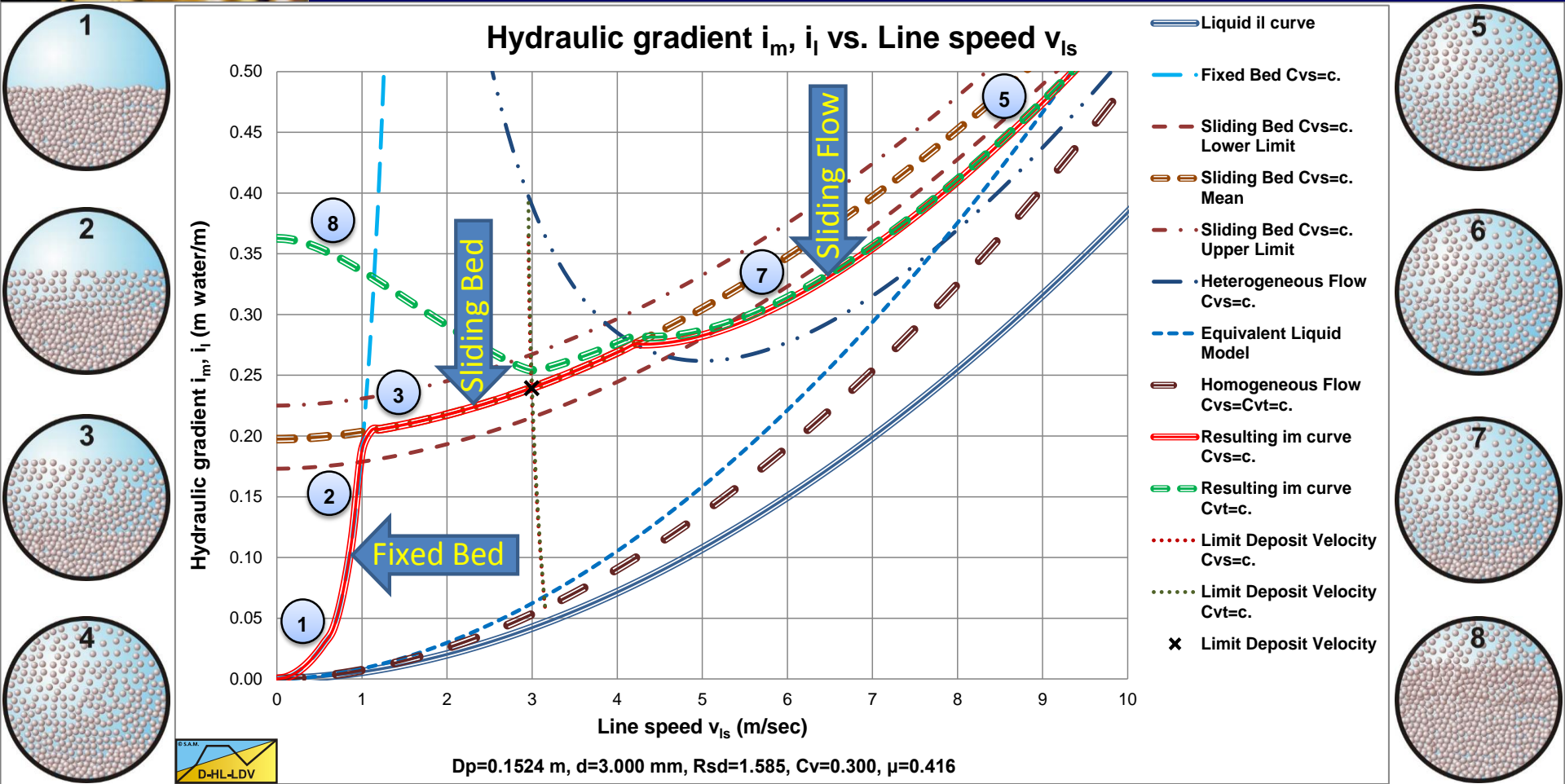
Scenario L2B & R2B, $i_m - v_{ls}$



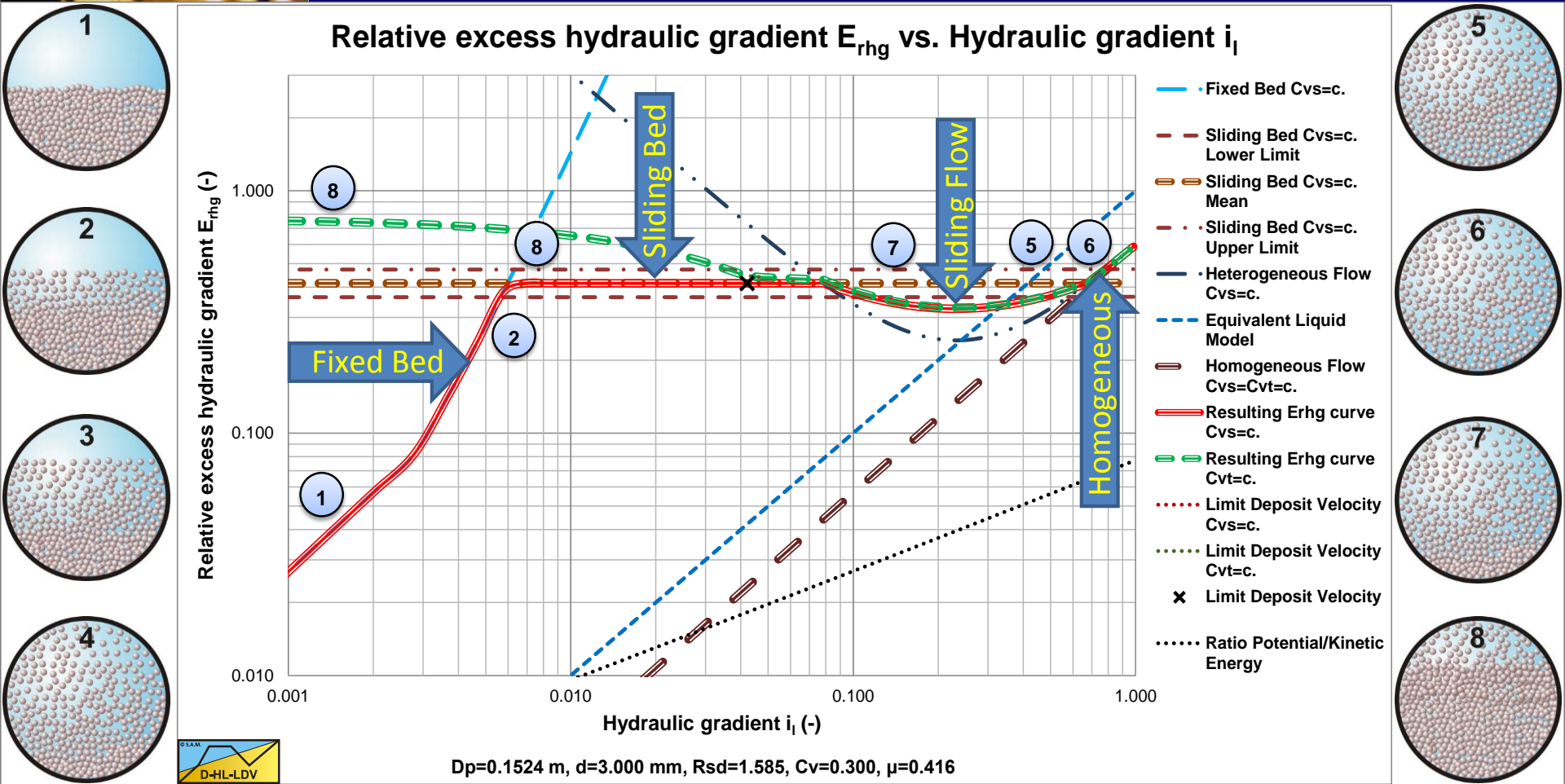
Scenario L2B & R2B, $E_{rhg}-i_1$



Scenario L3 & R3, $i_m - v_{ls}$



Scenario L3 & R3, $E_{rhg}-i_1$

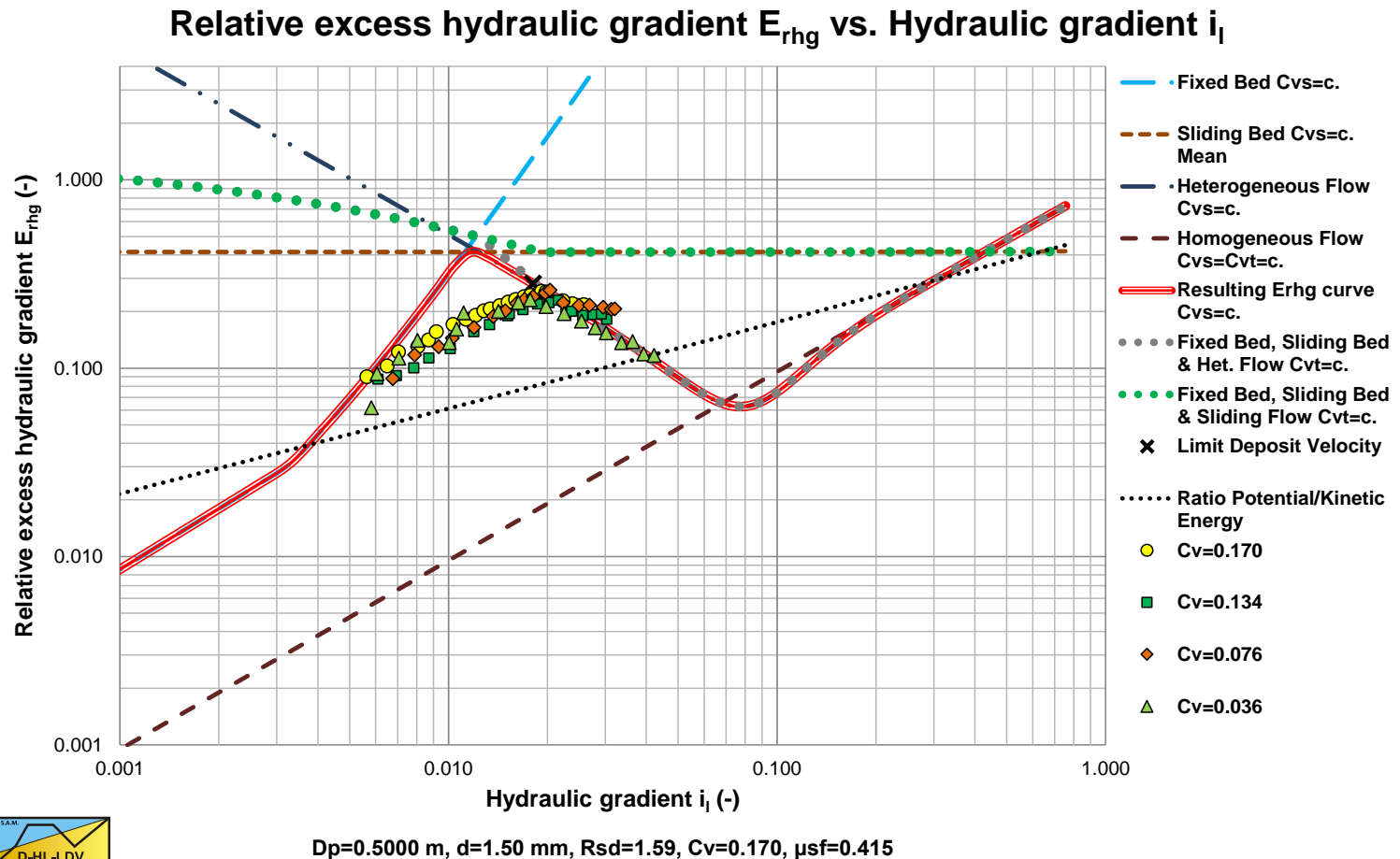




Verification/Validation Experiments

Chapter 7.2

Fixed Bed – Heterogeneous

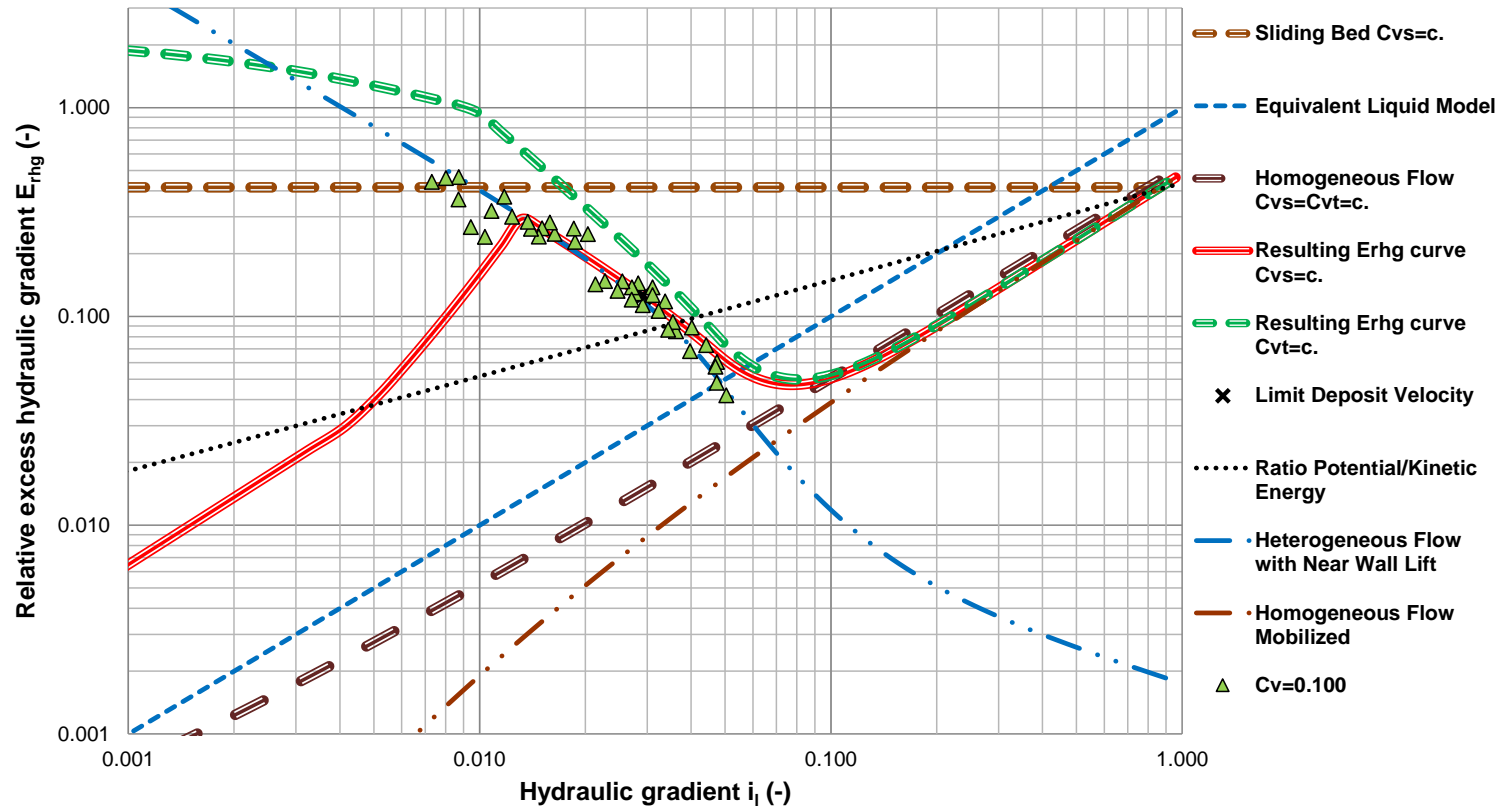


Kazanskij (1980), $C_{vs}=c.$

Delft University of Technology – Offshore & Dredging Engineering

Heterogeneous

Relative excess hydraulic gradient E_{rhg} vs. Hydraulic gradient i_i

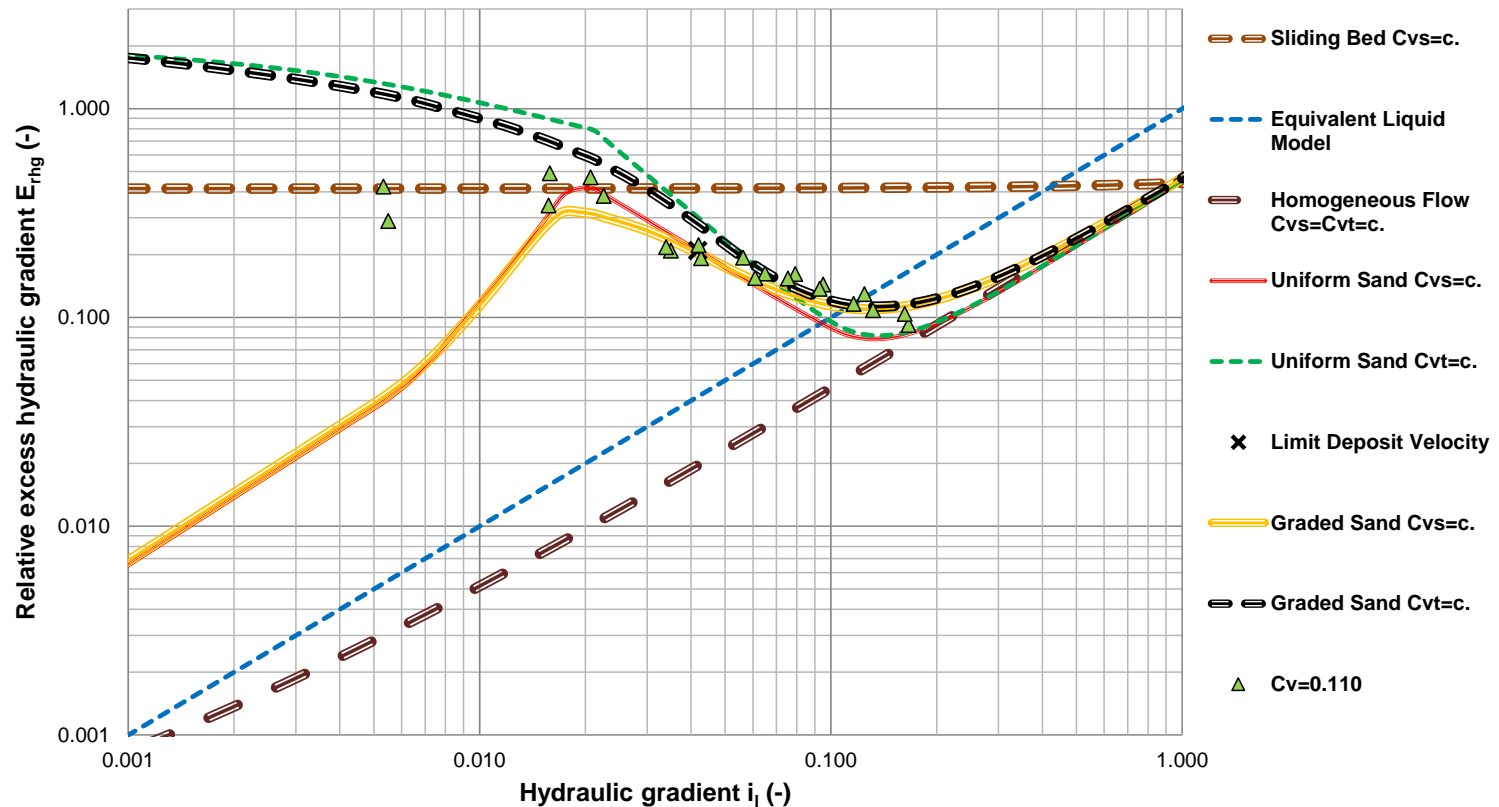


$D_p=0.4400$ m, $d=0.680$ mm, $R_{sd}=1.585$, $C_v=0.100$, $\mu_{sf}=0.416$

Clift (1982), $C_{vt}=c$.

Heterogeneous

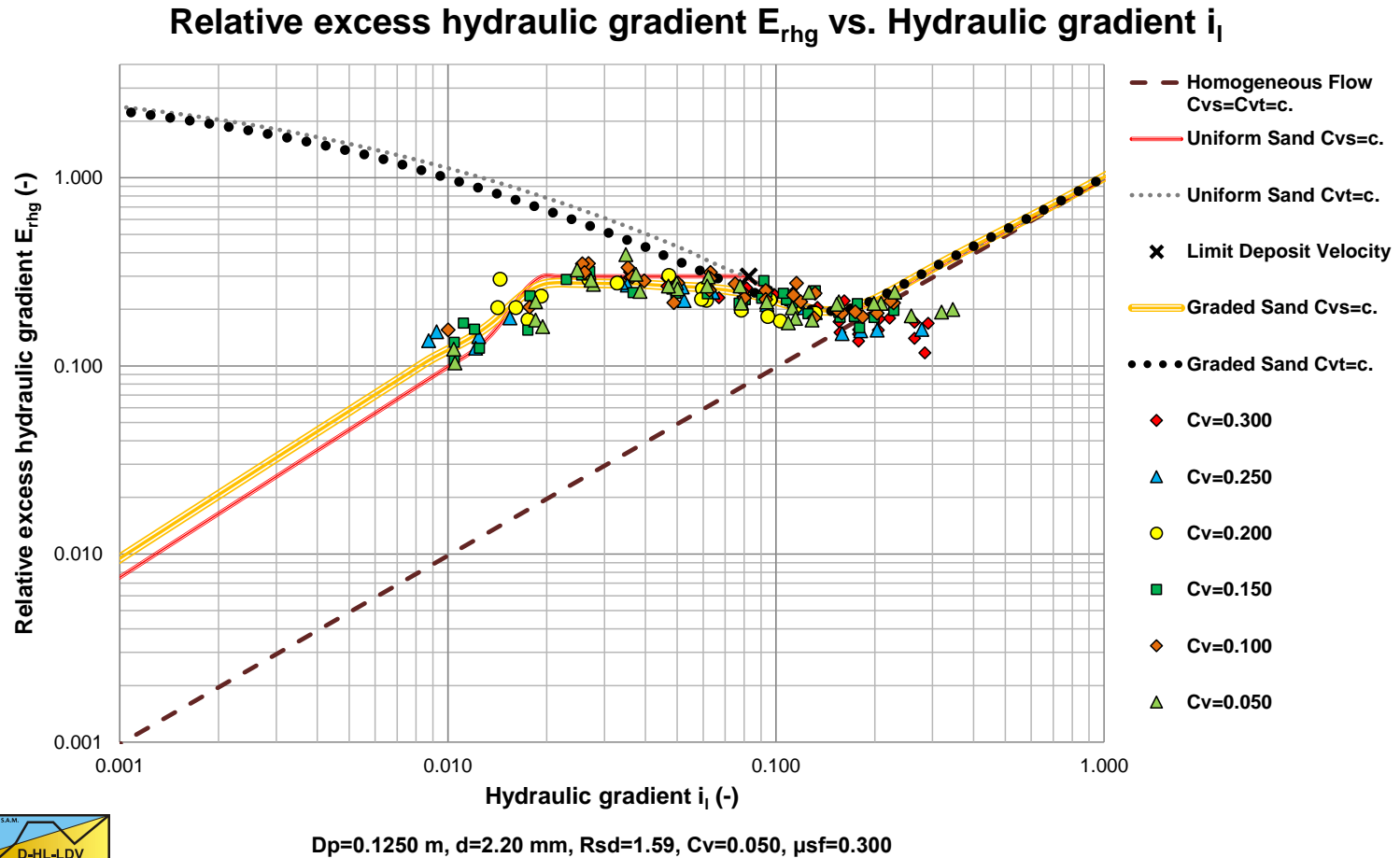
Relative excess hydraulic gradient E_{rhg} vs. Hydraulic gradient i_i



$D_p=0.2032$ m, $d=0.681$ mm, $R_{sd}=1.585$, $C_v=0.110$, $\mu_{sf}=0.416$

Clift (1982), $C_{vt}=c$, Broad Graded.

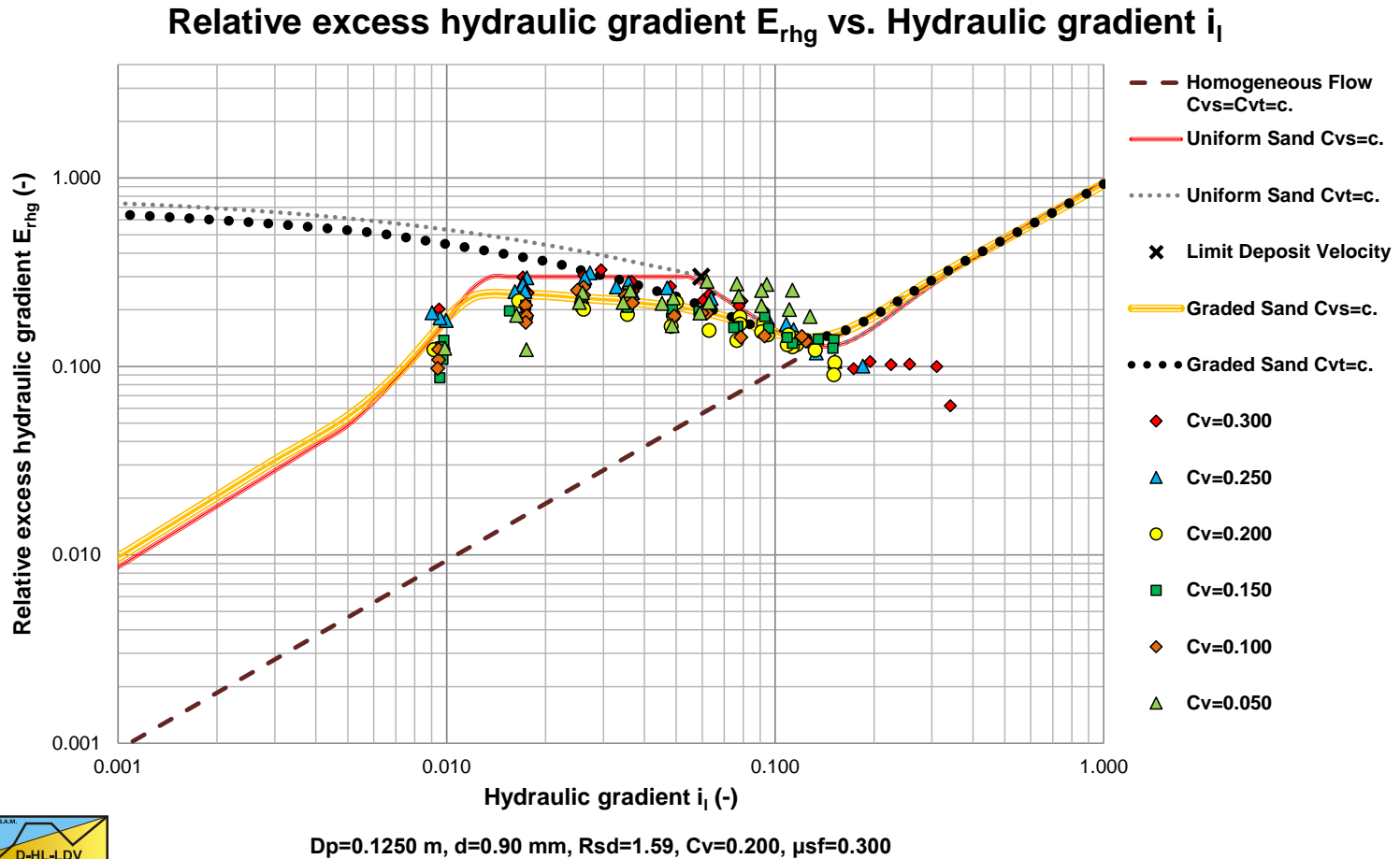
Fixed Bed - Sliding Bed - Heterogeneous



Wiedenroth (1967), $C_{vs}=c.$, Coarse Sand

Delft University of Technology – Offshore & Dredging Engineering

Fixed Bed - Sliding Bed - Heterogeneous

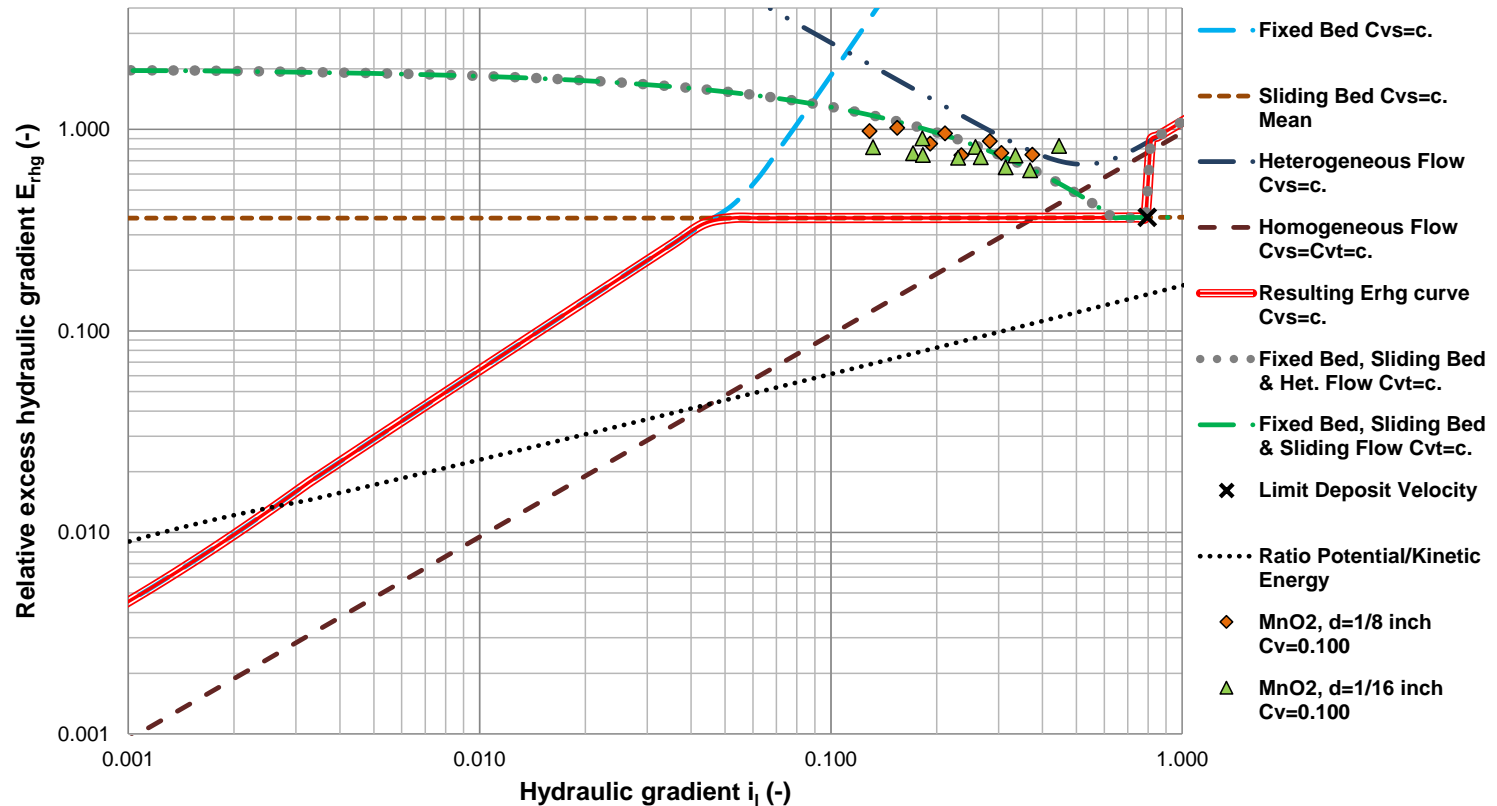


Wiedenroth (1967), $C_{vs}=c.$, Medium Sand

Delft University of Technology – Offshore & Dredging Engineering

Sliding Bed

Relative excess hydraulic gradient E_{rhg} vs. Hydraulic gradient i_i



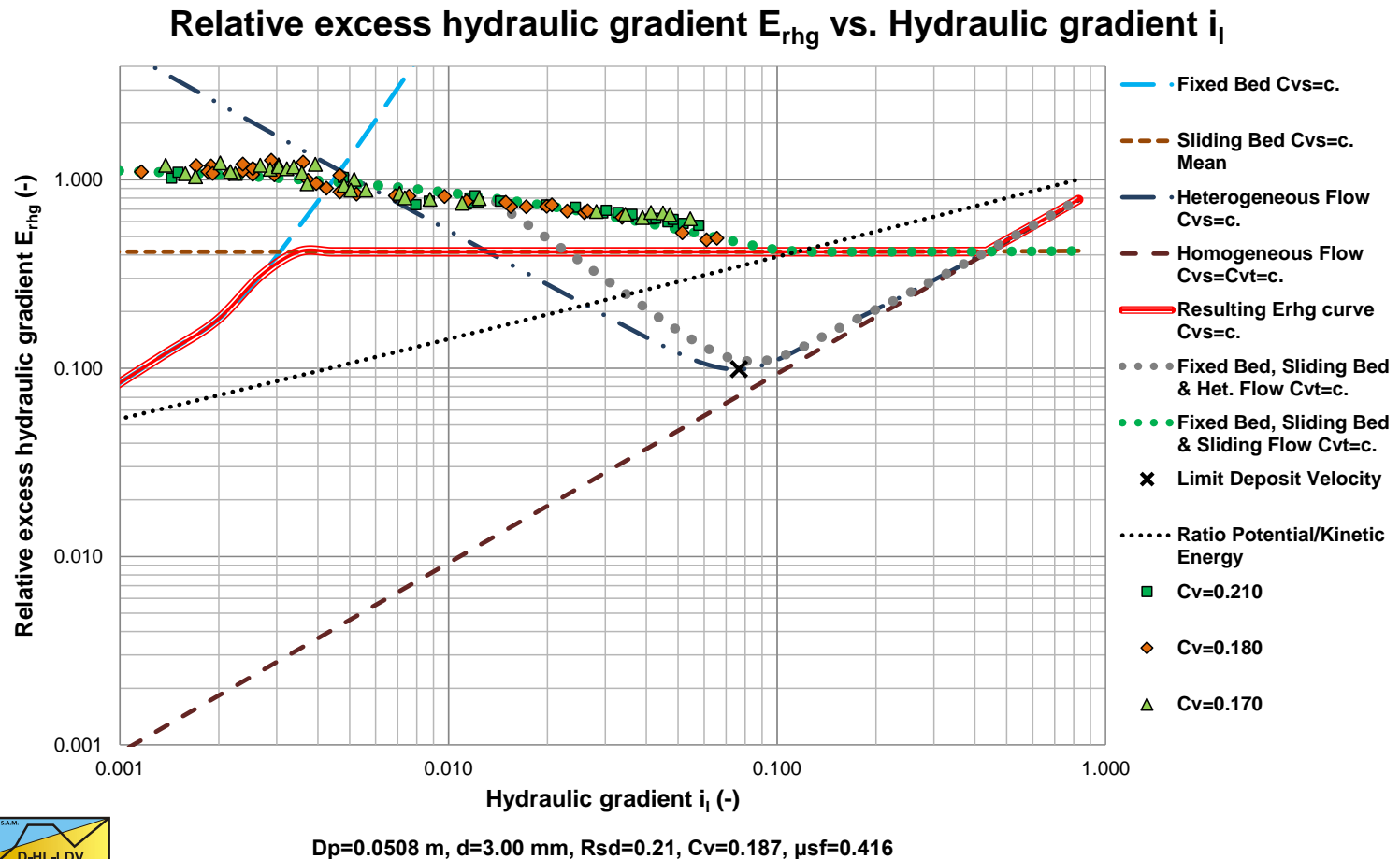
$D_p=0.0254$ m, $d=3.00$ mm, $R_{sd}=3.00$, $C_v=0.100$, $\mu_{sf}=0.364$



Newitt et al. (1955), $C_{vt}=c.$, MnO₂

Delft University of Technology – Offshore & Dredging Engineering

Sliding Bed, Sliding Flow



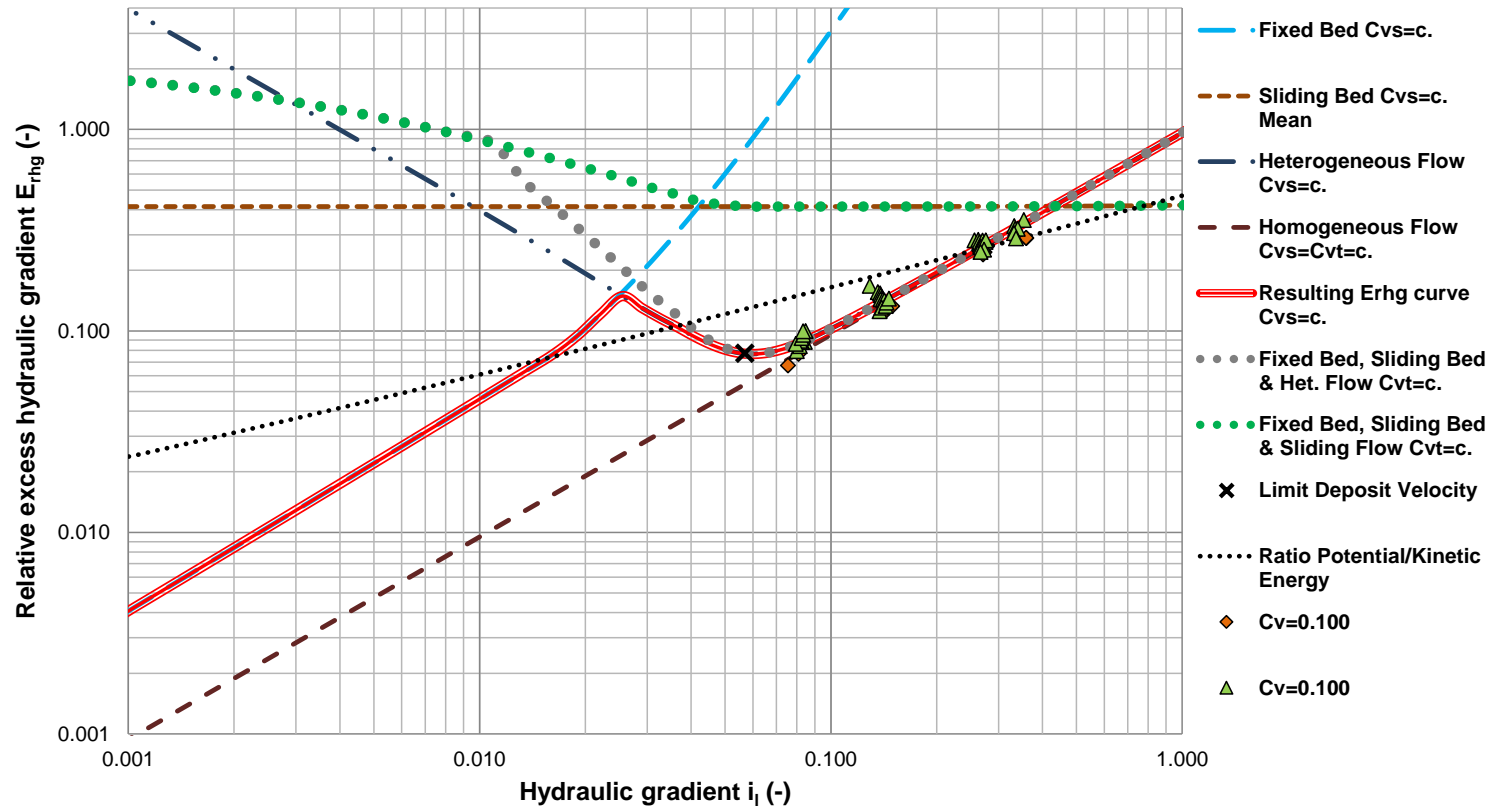
Doron & Barnea (1993), $C_{vt}=c$, Acetal

Delft University of Technology – Offshore & Dredging Engineering



Homogeneous

Relative excess hydraulic gradient E_{rhg} vs. Hydraulic gradient i_i

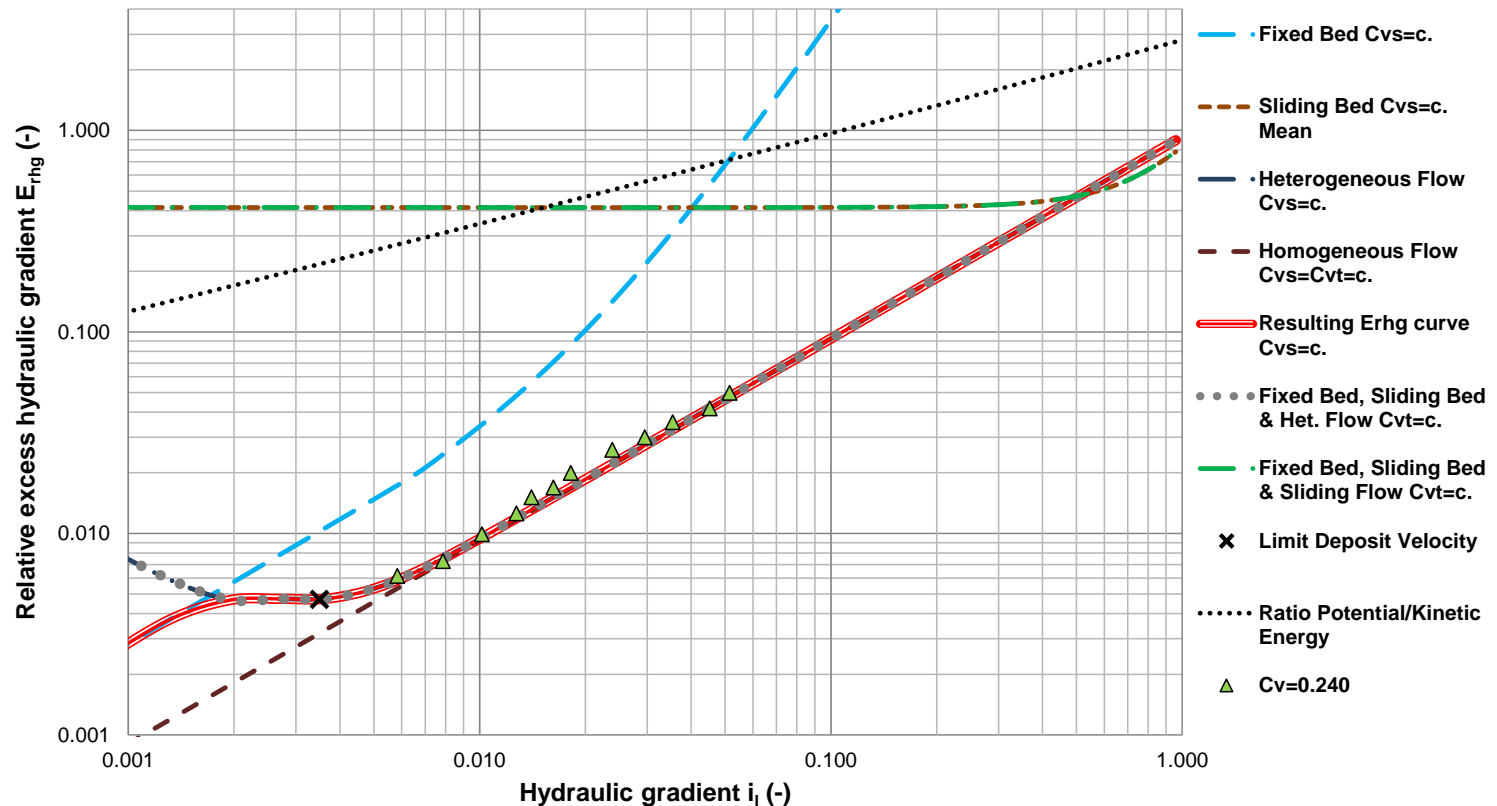


$D_p=0.0254$ m, $d=0.16$ mm, $R_{sd}=1.59$, $C_v=0.100$, $\mu_{sf}=0.415$

Babcock (1970)

Homogeneous

Relative excess hydraulic gradient E_{rhg} vs. Hydraulic gradient i_i



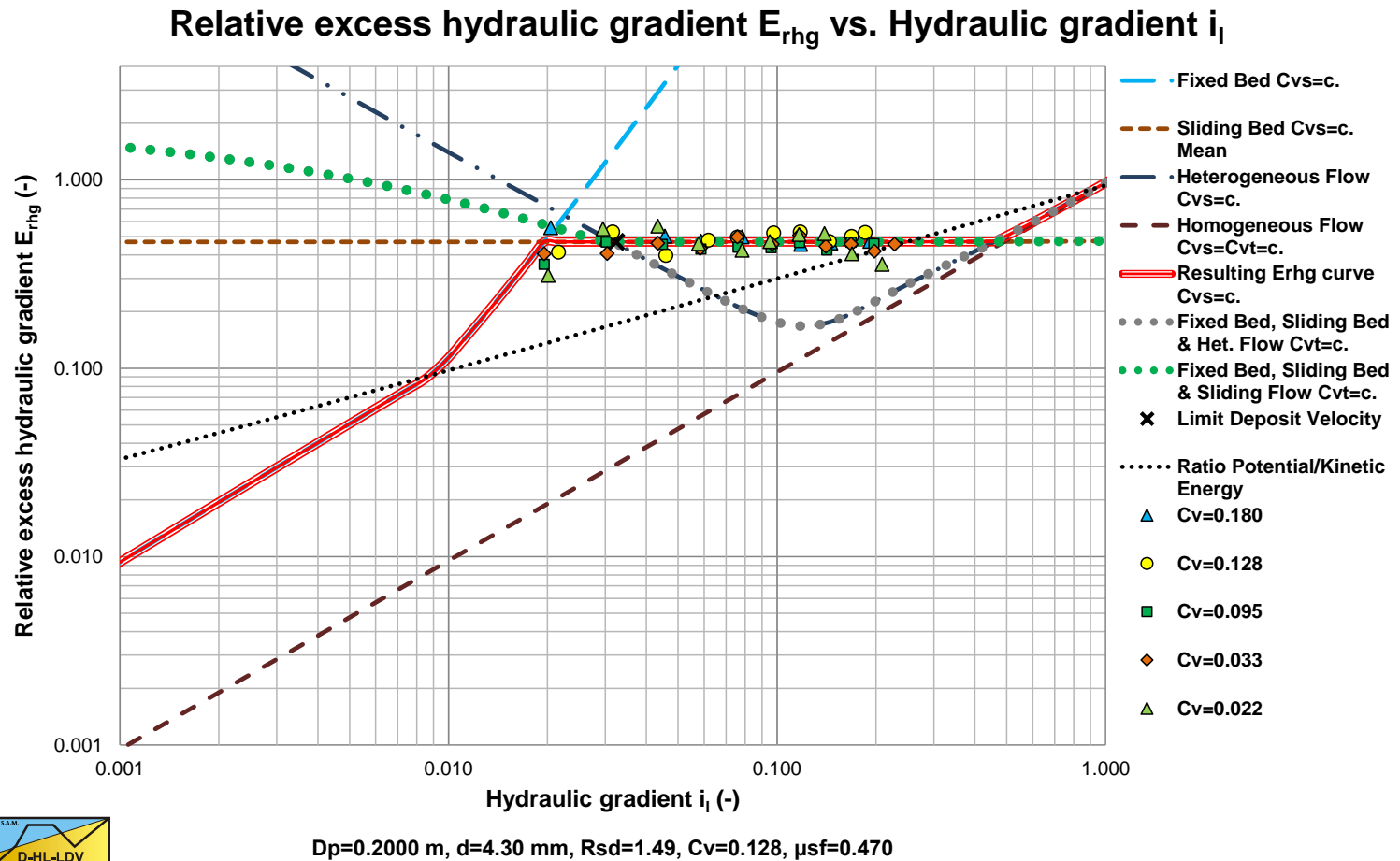
$D_p=0.1585$ m, $d=0.04$ mm, $R_{sd}=4.00$, $C_v=0.240$, $\mu_{sf}=0.415$

Thomas (1976), Iron Ore

Delft University of Technology – Offshore & Dredging Engineering



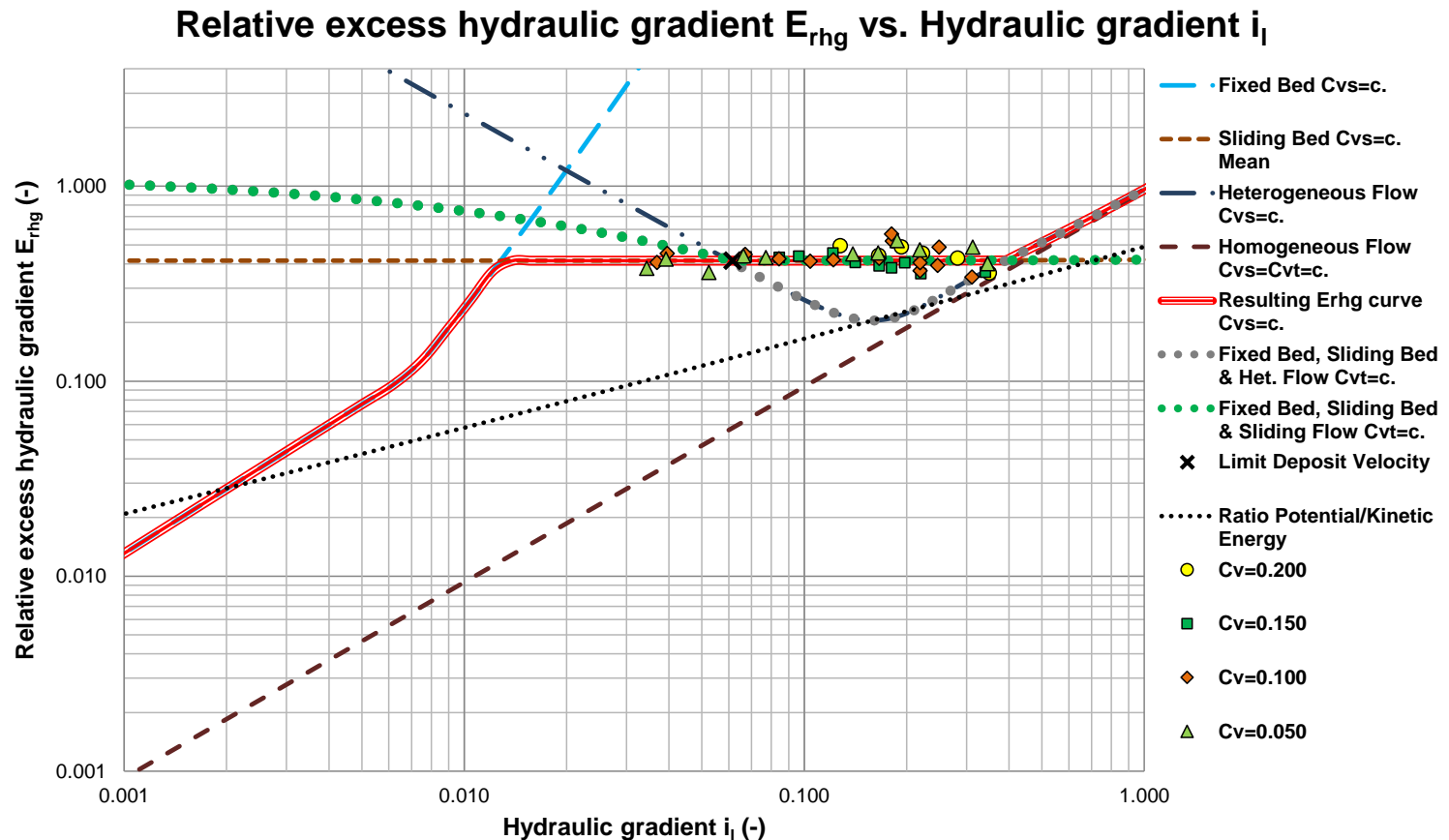
Fixed Bed – Sliding Bed – Sliding Flow



Boothroyde (1979), $C_{vs}=c.$

Delft University of Technology – Offshore & Dredging Engineering

Fixed Bed – Sliding Bed – Sliding Flow



$D_p=0.1250$ m, $d=4.45$ mm, $R_{sd}=1.59$, $C_v=0.200$, $\mu_{sf}=0.416$

Wiedenroth (1967), $C_{vs}=c.$, Gravel

Delft University of Technology – Offshore & Dredging Engineering



Transition Line Speed Heterogeneous – Homogeneous

Chapter 9

The Transition Line Speed Heterogeneous-Homogeneous

Problem definition:

For slurry transport in general and specifically in dredging, there are many models. But how to decide which model to use in which situation, or, when are specific models valid especially in the heterogeneous flow regime.

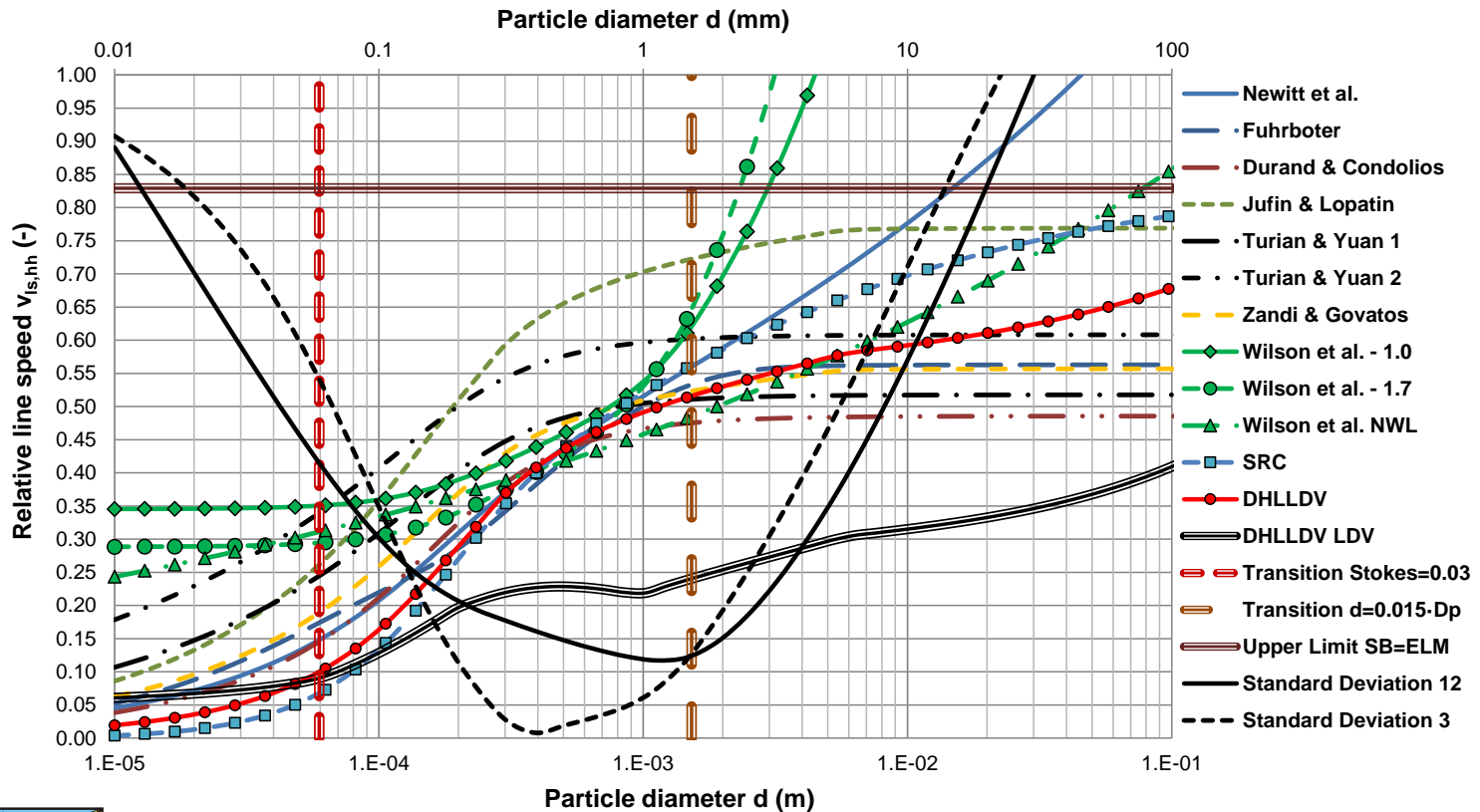
Solution:

The transition line speed of the heterogeneous flow regime with the homogeneous flow regime is a good indicator and limits the number of graphs.

Relative Transition Line Speed

$D_p=0.1016 \text{ m}, C_{vs}=0.05$

Transition Heterogeneous - Homogeneous



$D_p=0.1016 \text{ m}, R_{sd}=1.585, C_{vs}=0.050, \mu_{sf}=0.416$

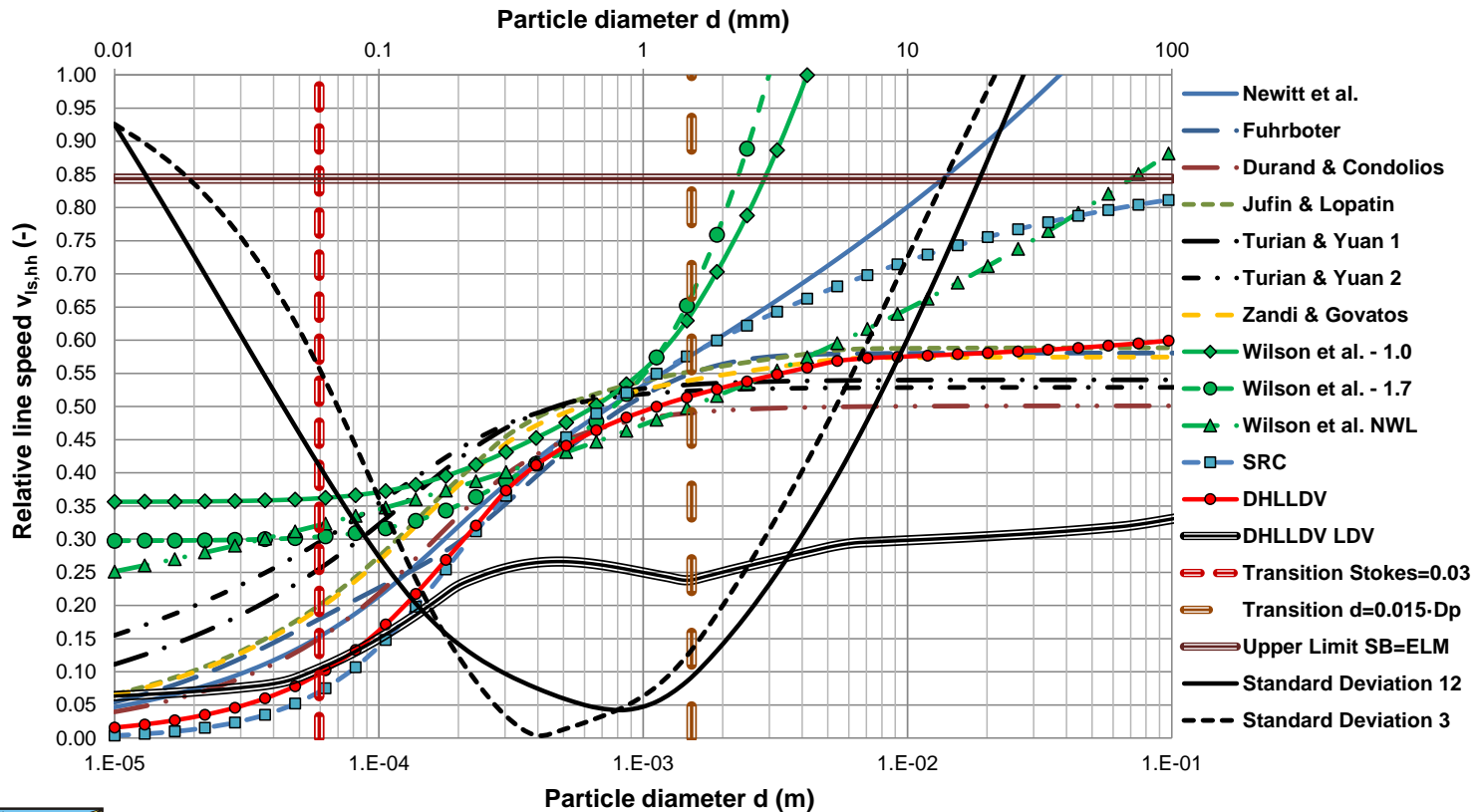
$v_{ls,hh,max}=9.8 \text{ m/sec}$



Relative Transition Line Speed

$D_p=0.1016 \text{ m}, C_{vs}=0.30$

Transition Heterogeneous - Homogeneous



$D_p=0.1016 \text{ m}, R_{sd}=1.585, C_{vs}=0.300, \mu_{sf}=0.416$

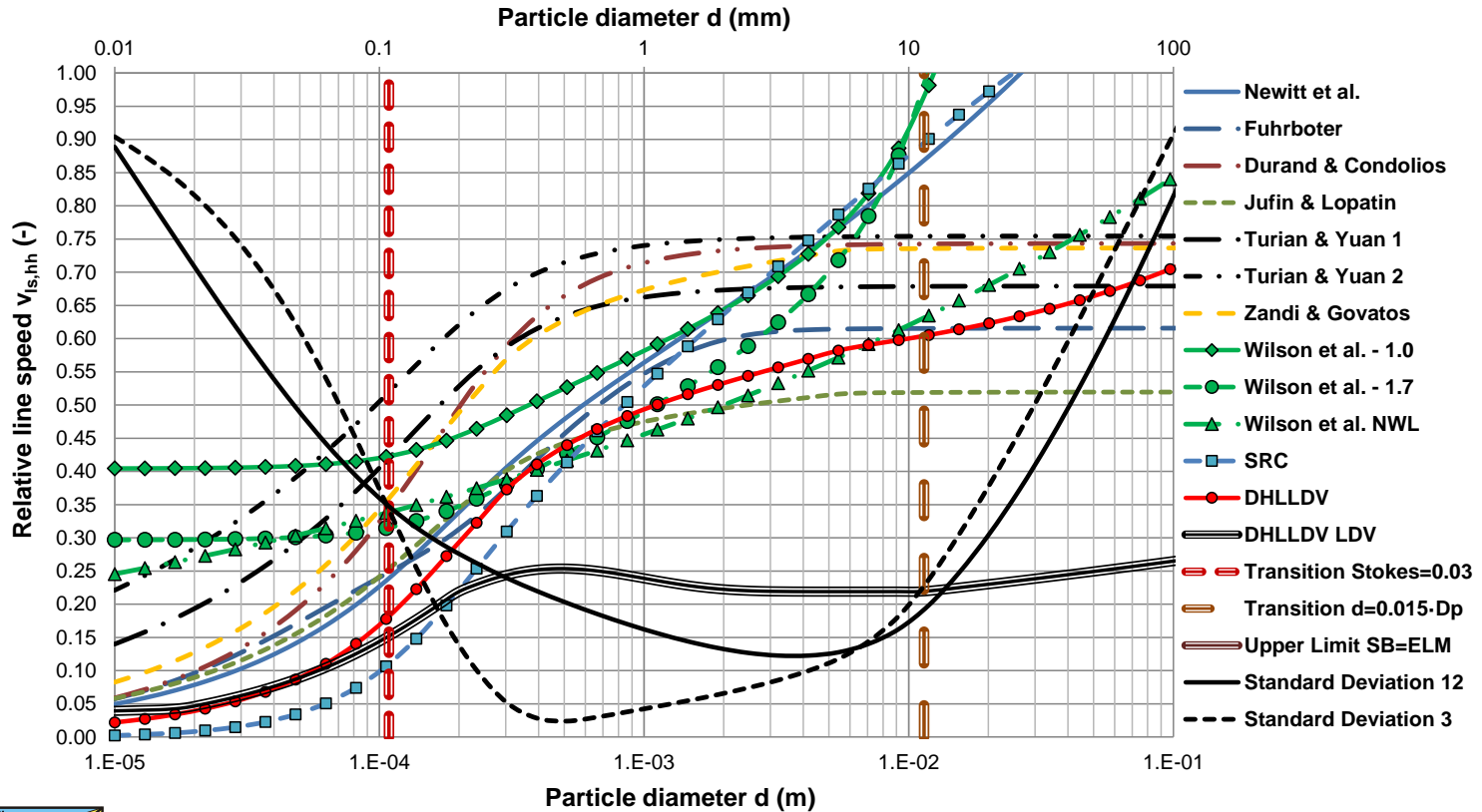
$v_{ls,hh,max}=9.5 \text{ m/sec}$



Relative Transition Line Speed

$D_p = 0.7620 \text{ m}, C_{vs} = 0.05$

Transition Heterogeneous - Homogeneous



$D_p = 0.7620 \text{ m}, R_{sd} = 1.585, C_{vs} = 0.050, \mu_{sf} = 0.416$

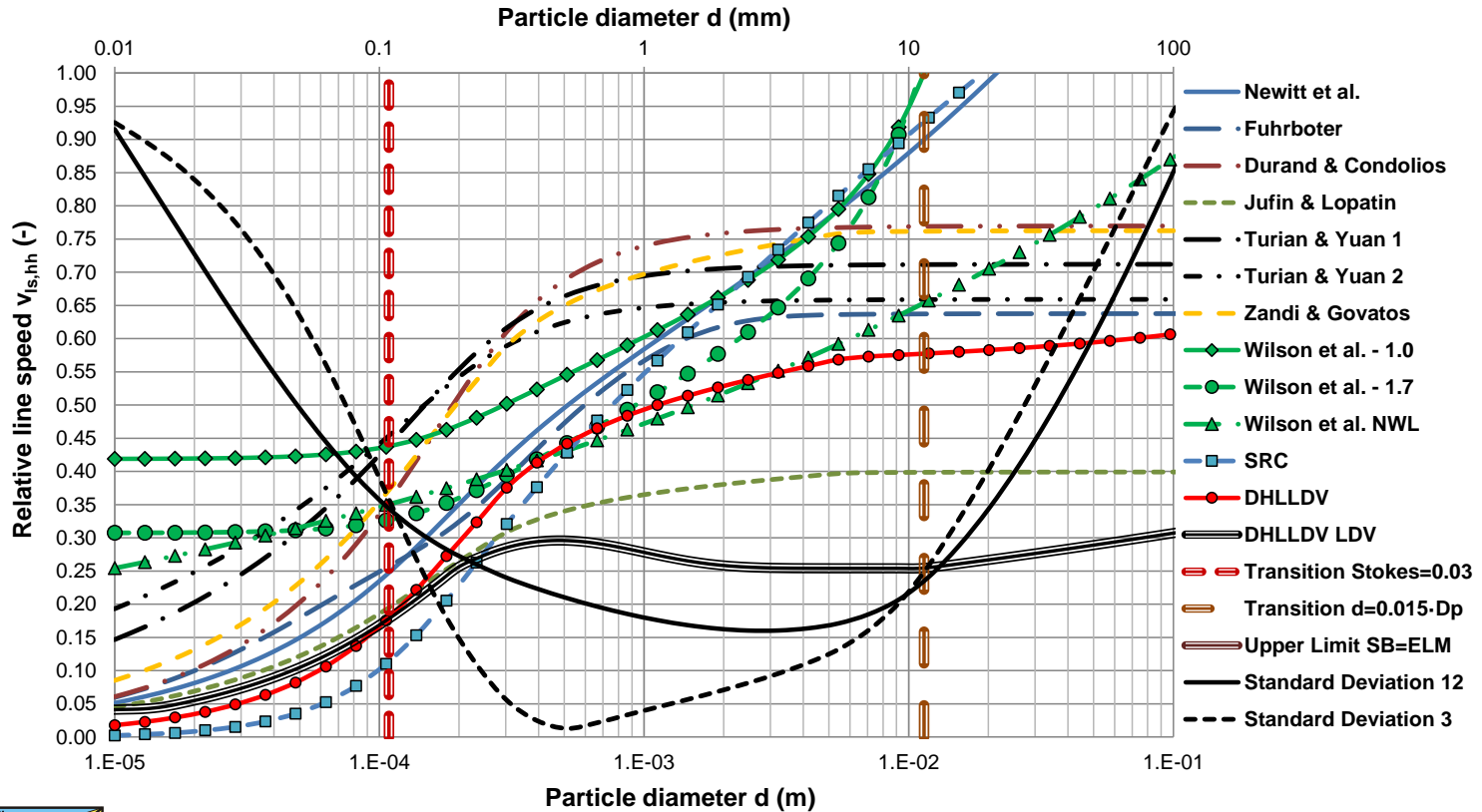
$v_{ls,hh,max} = 20.3 \text{ m/sec}$



Relative Transition Line Speed

$D_p=0.7620$ m, $C_{vs}=0.30$

Transition Heterogeneous - Homogeneous

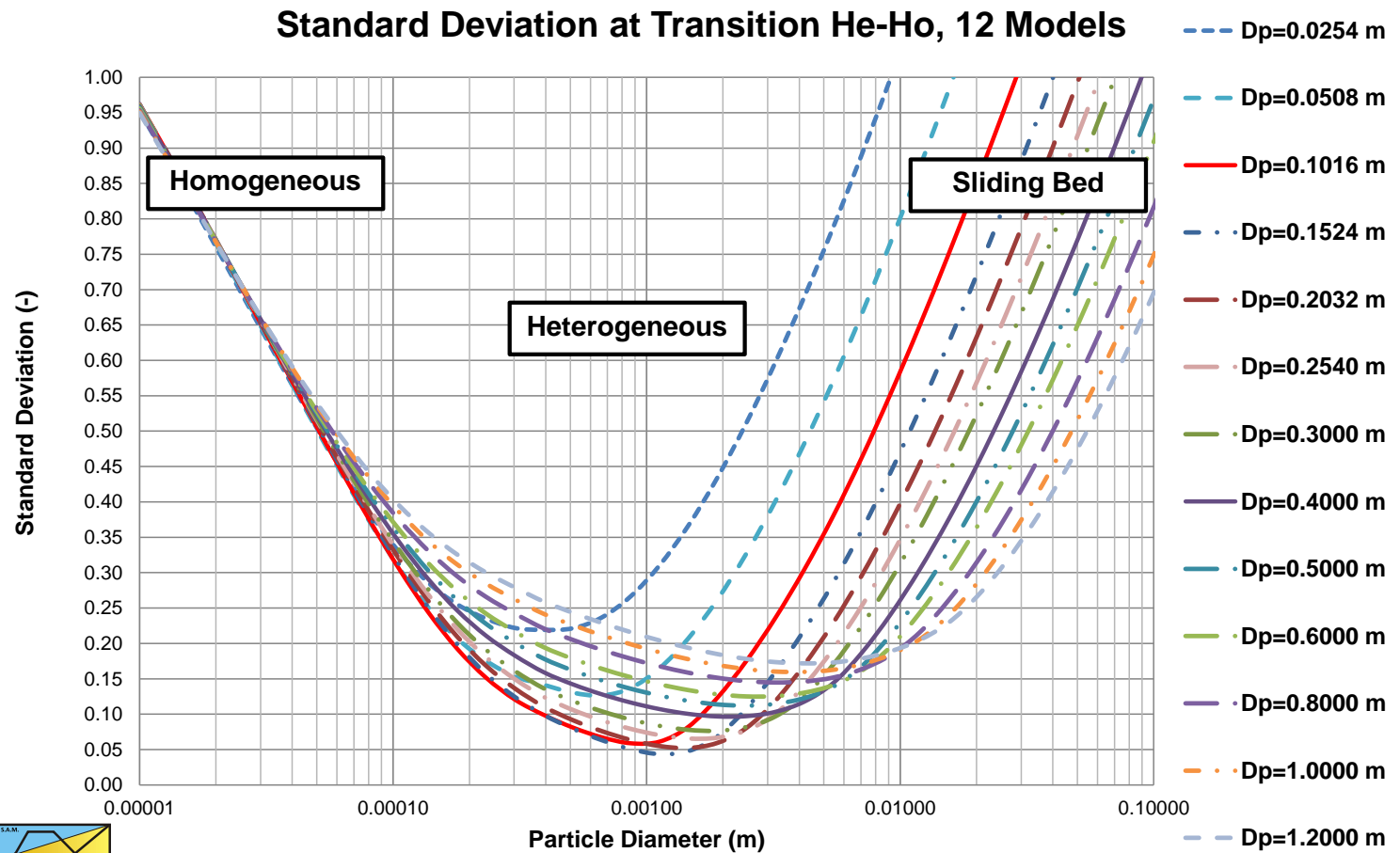


$D_p=0.7620$ m, $R_{sd}=1.585$, $C_{vs}=0.300$, $\mu_{sf}=0.416$

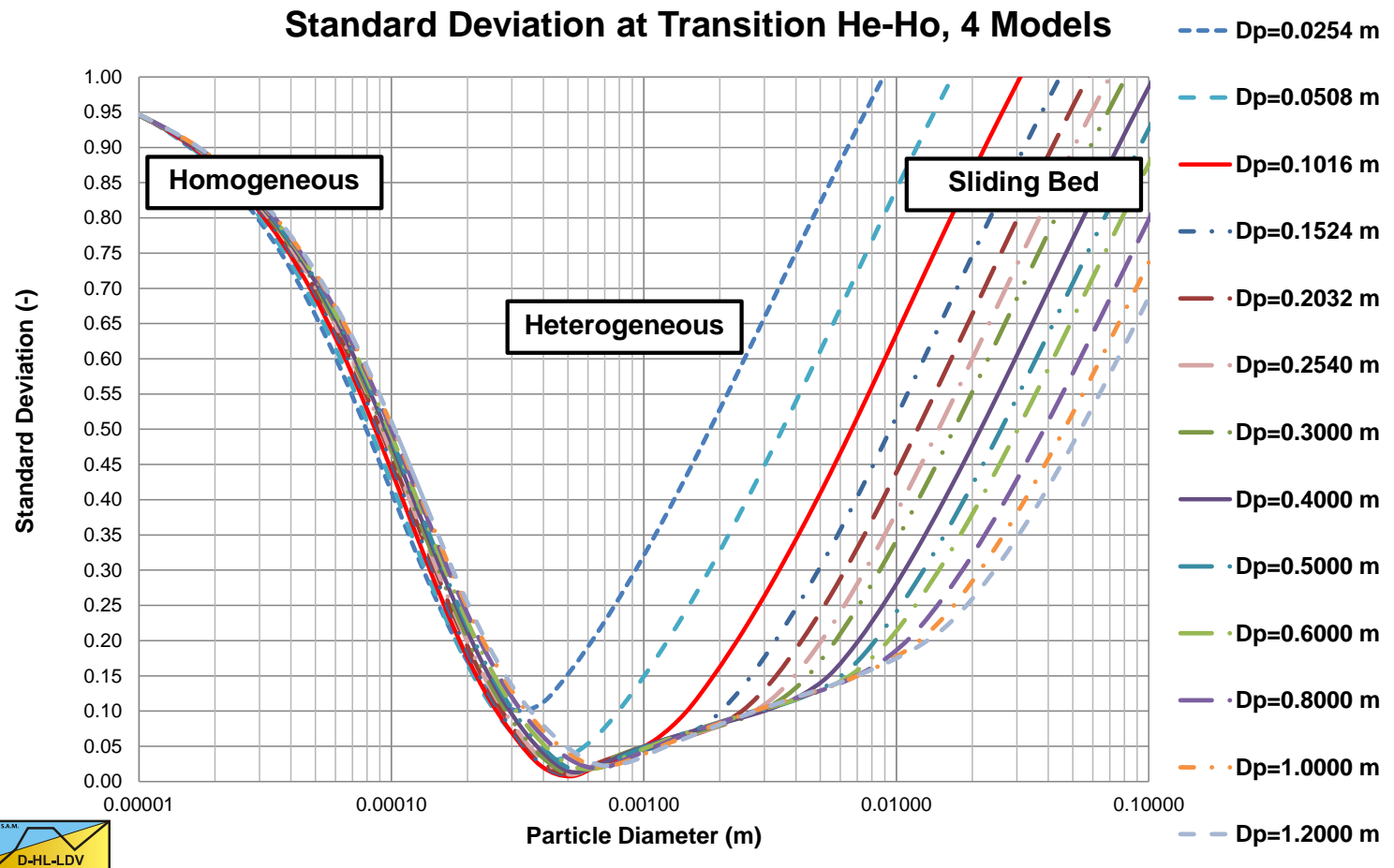
$v_{ls,hh,max}=19.6$ m/sec



Standard Deviation 12 Models



Standard Deviation DHLLDV-Wilson/SRC

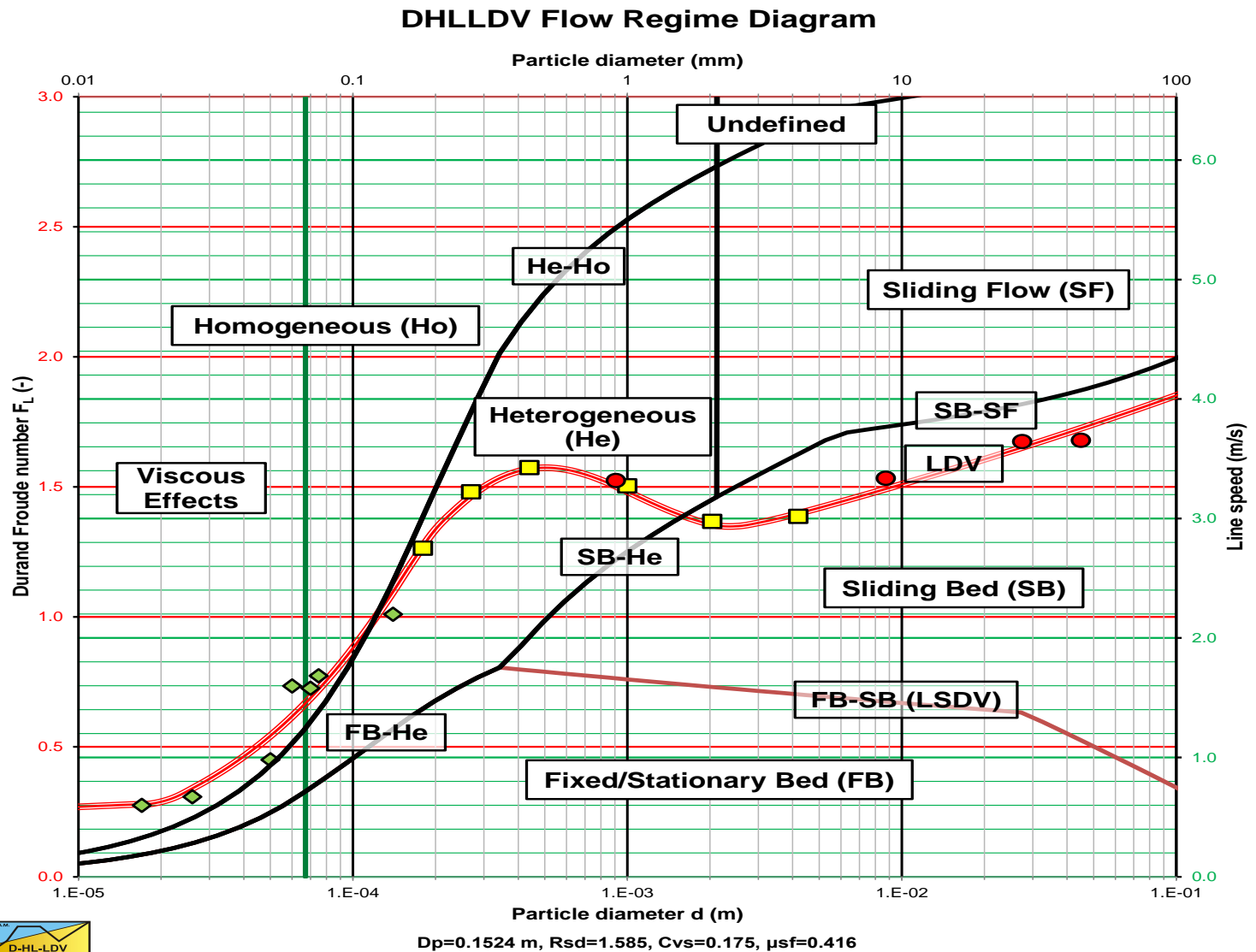




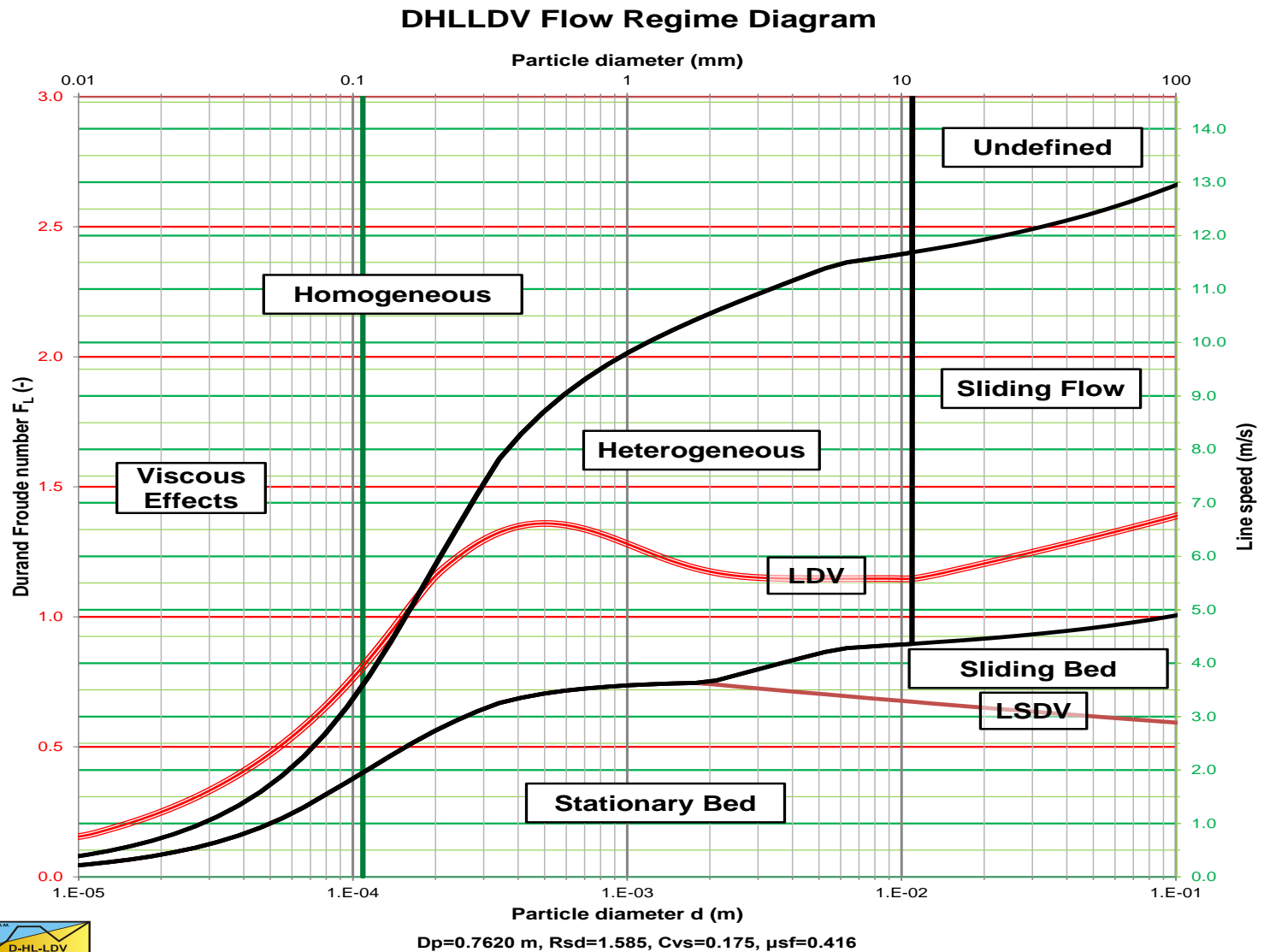
Flow Regime Diagrams

Chapter 7.8 & Appendix D

Small Pipe Diameter, $C_{vs}=0.175$



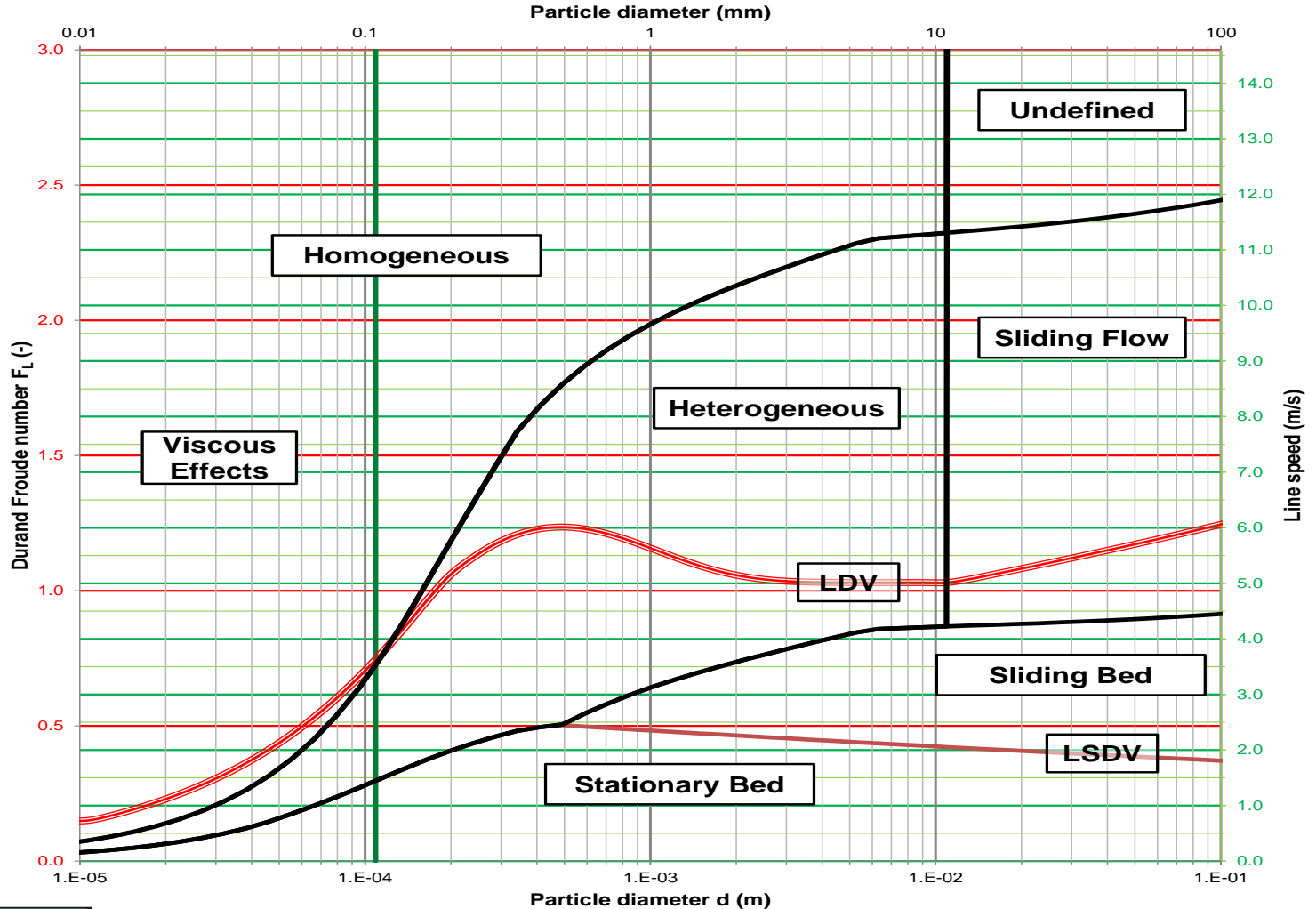
A Large Diameter Pipe, $C_{vs}=0.175$



A Large Diameter Pipe, $C_{vs} = 0.3$



DHLLDV Flow Regime Diagram



$D_p = 0.7620$ m, $R_{sd} = 1.585$, $C_{vs} = 0.300$, $\mu_{sf} = 0.416$



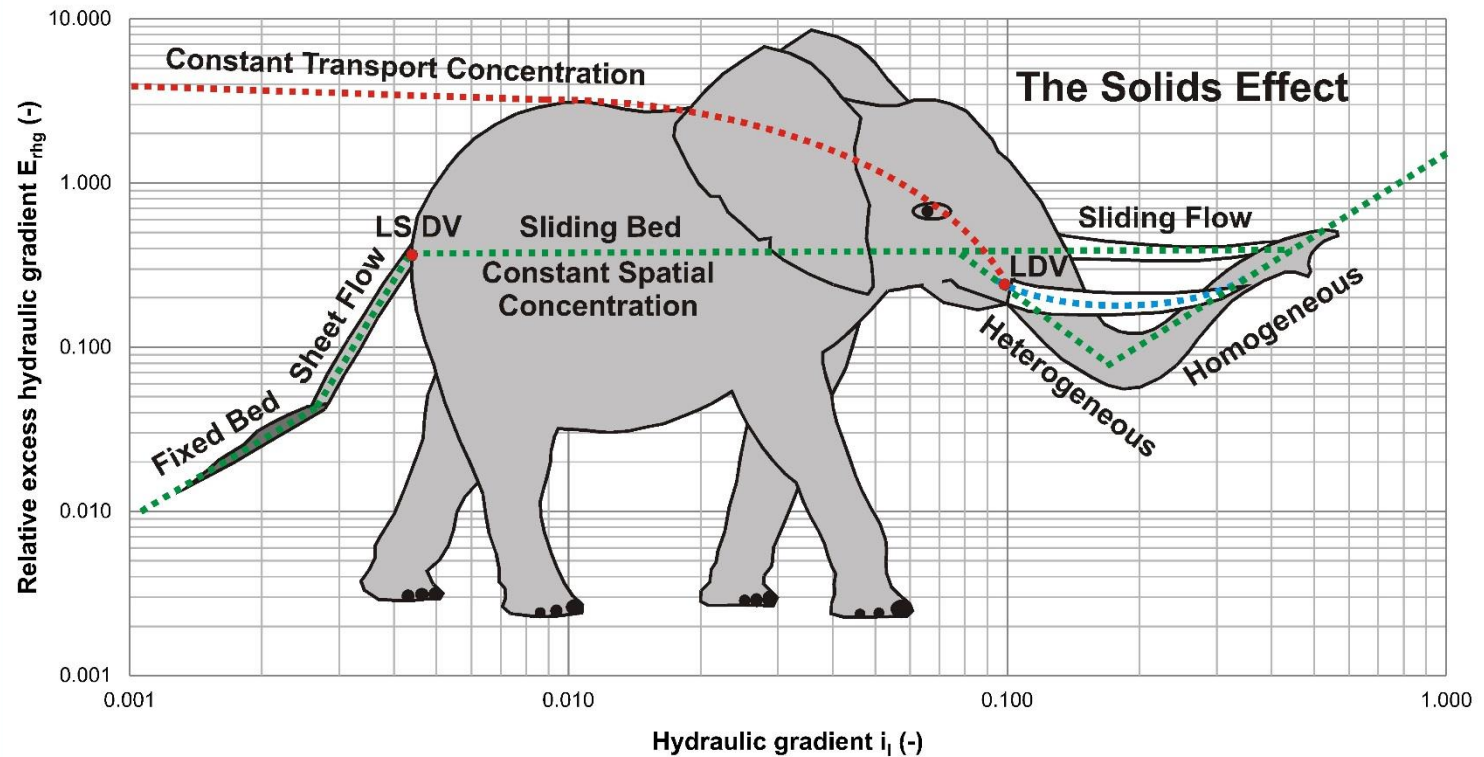


Conclusions

Leeghwater



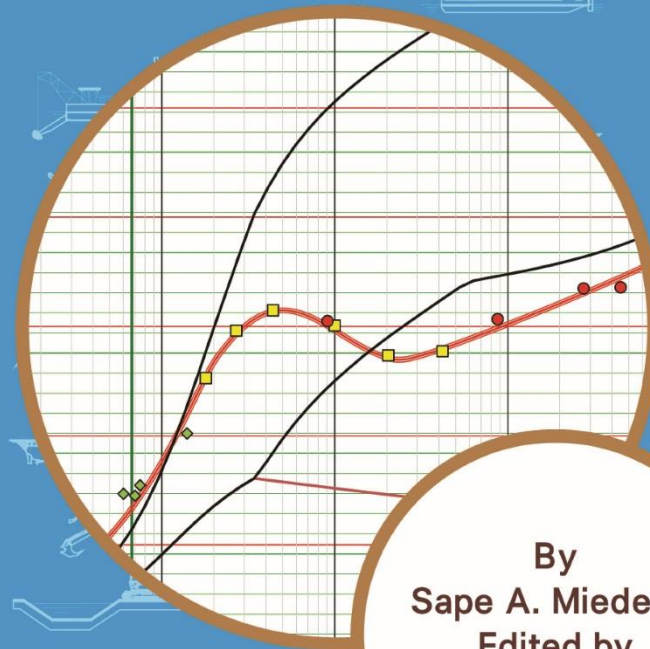
The **DHLLDV** Framework The Double Logarithmic Elephant: Leeghwater





SLURRY TRANSPORT

Fundamentals, A Historical Overview
& The Delft Head Loss & Limit
Deposit Velocity Framework



By
Sape A. Miedema
Edited by
Robert C. Ramsdell

The Elephant of Wilson is our best Friend

